

Process Integration and Intensification: A Fundamental Way for Decarbonization of Chemical Processes

(Mainly for Distillation Process)

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2024. 6. 19.

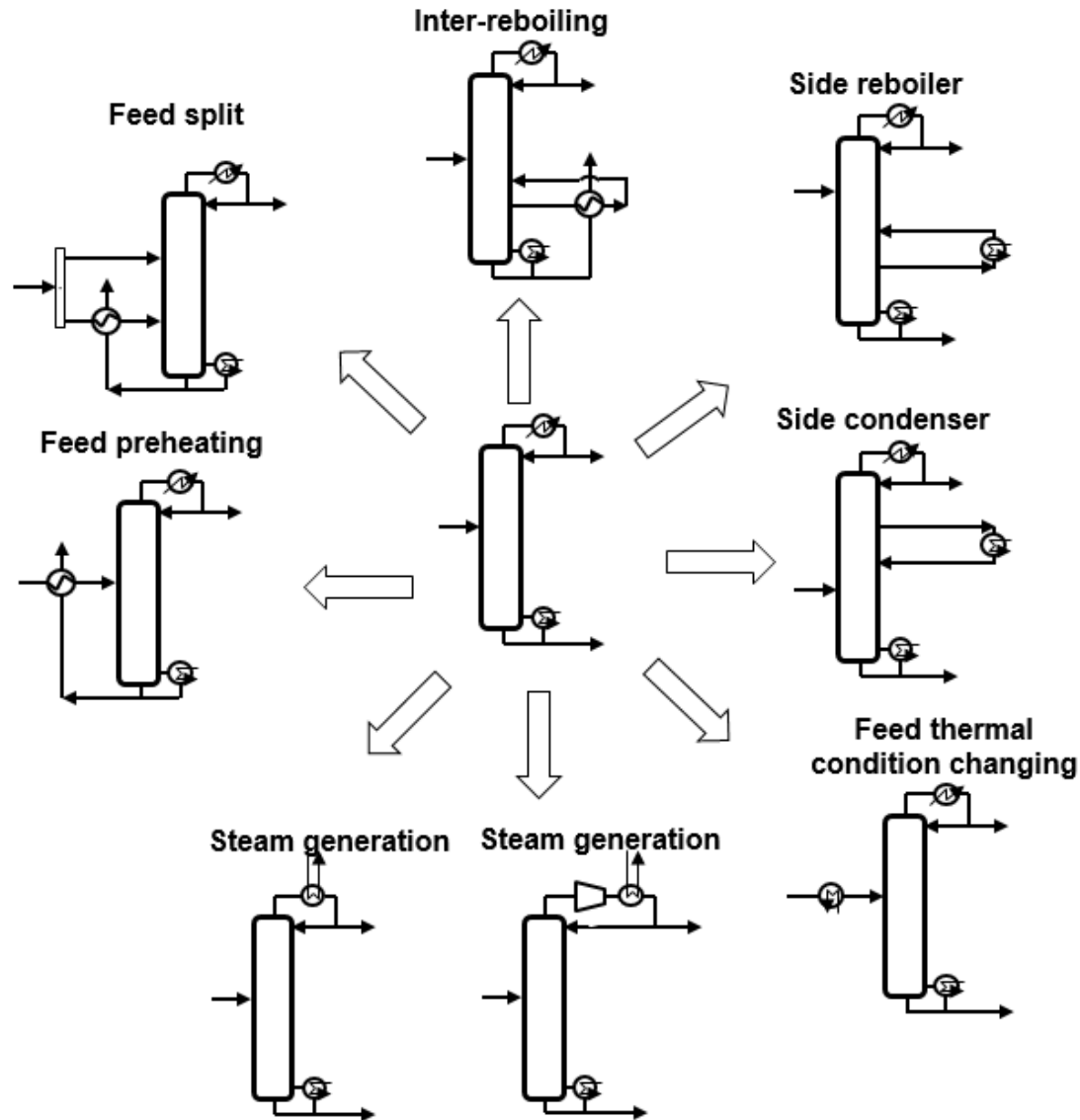
TNChE Asia 2024, Pataya, THAILAND

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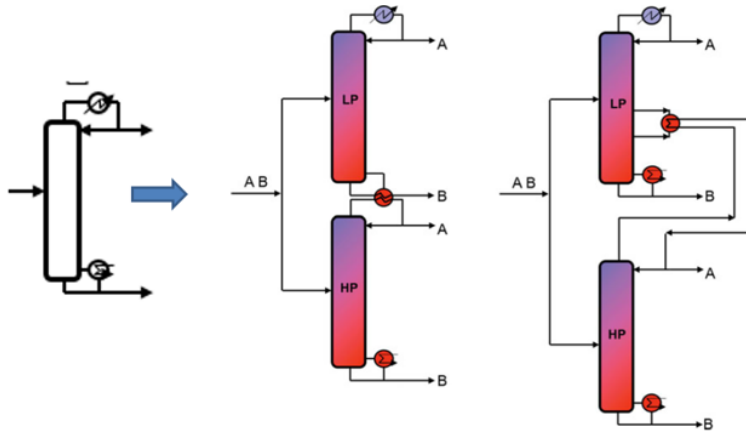
Heat Integrated Distillation

- Single Column with Two Products

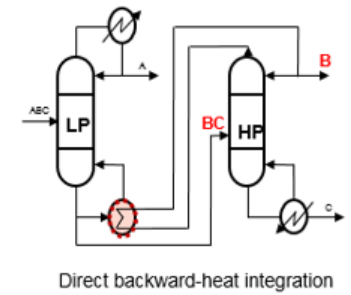
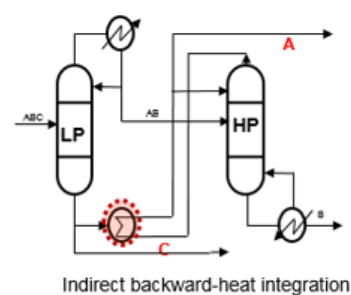
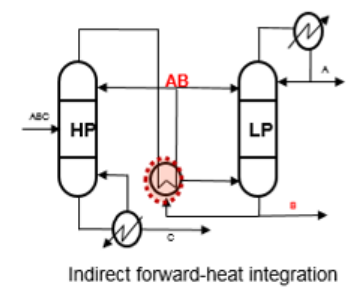
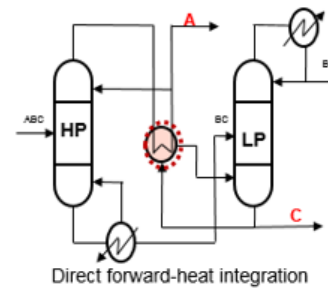
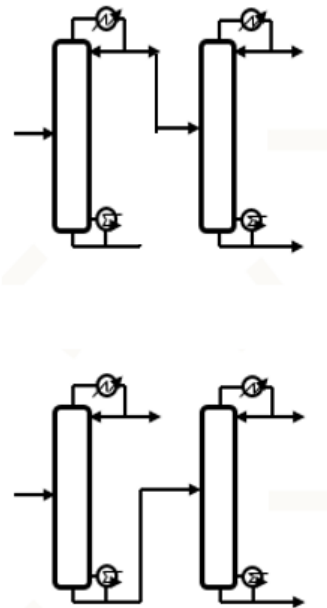


Heat Integrated Distillation

- Double-Effect Distillation (DED) for Single Column

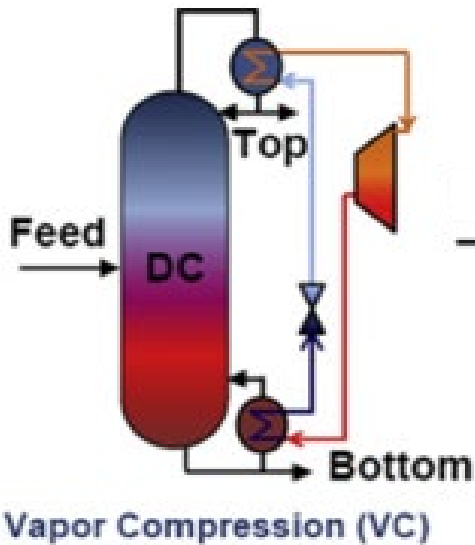
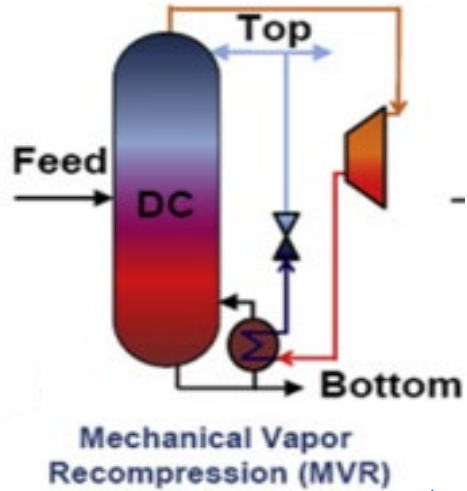
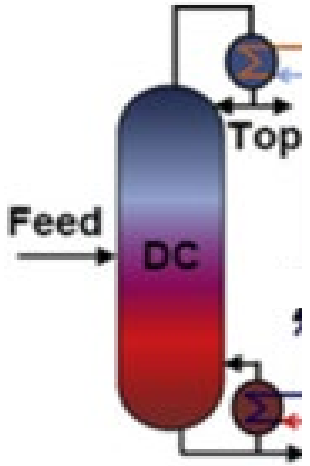


- Double-Effect Distillation (DED) for Two Columns

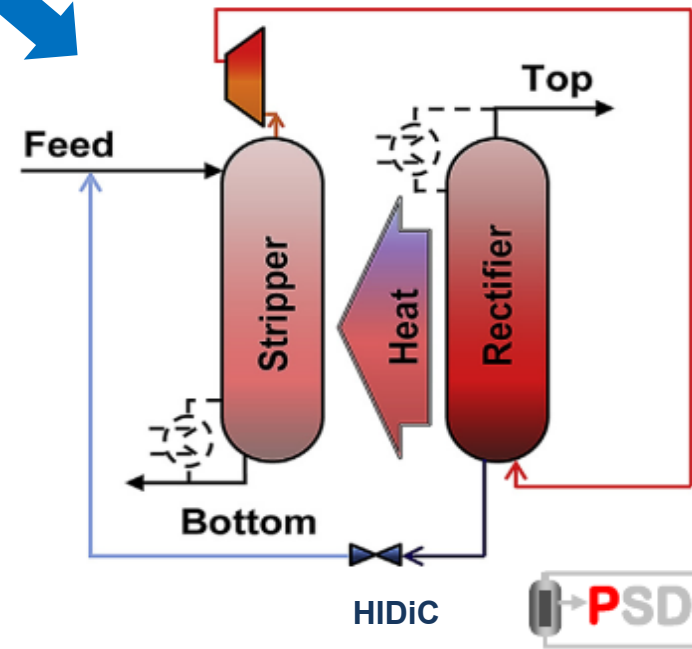


Heat Integrated Distillation

- Heat Pump Assisted Distillation: as a more aggressive way

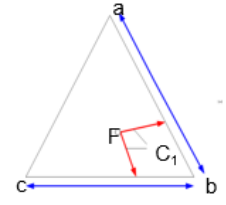
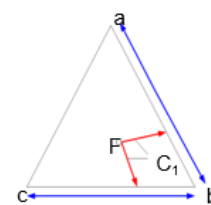
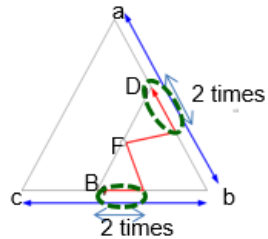
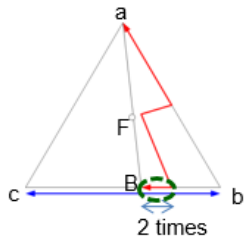
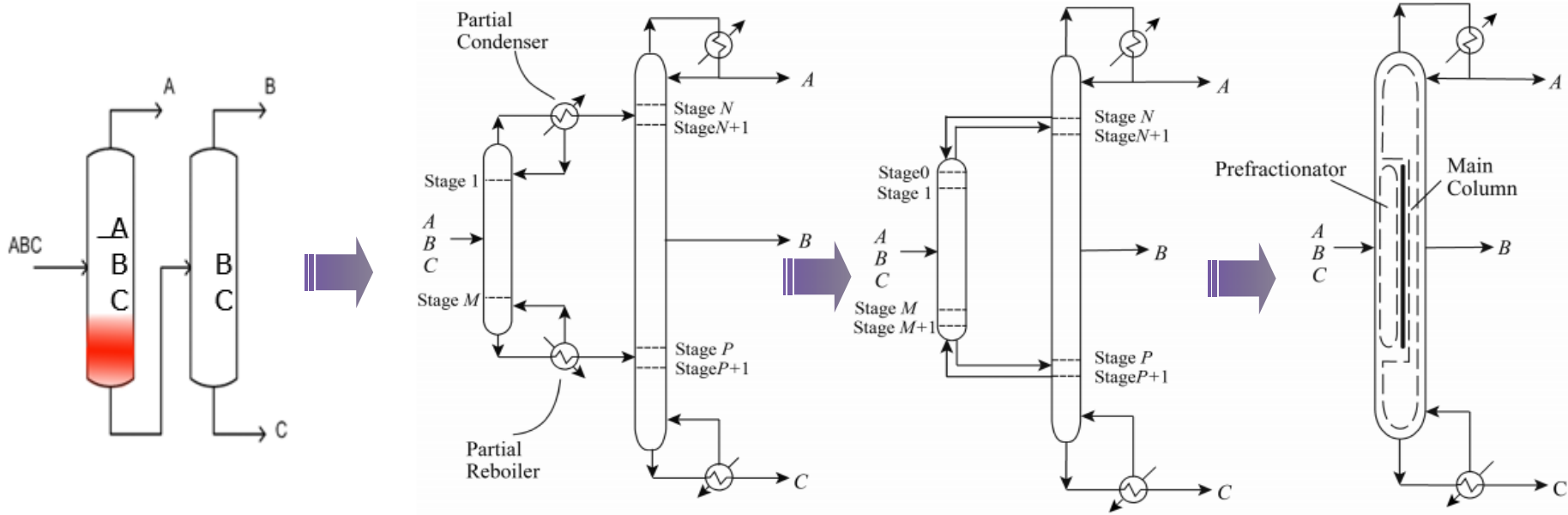


coming soon?

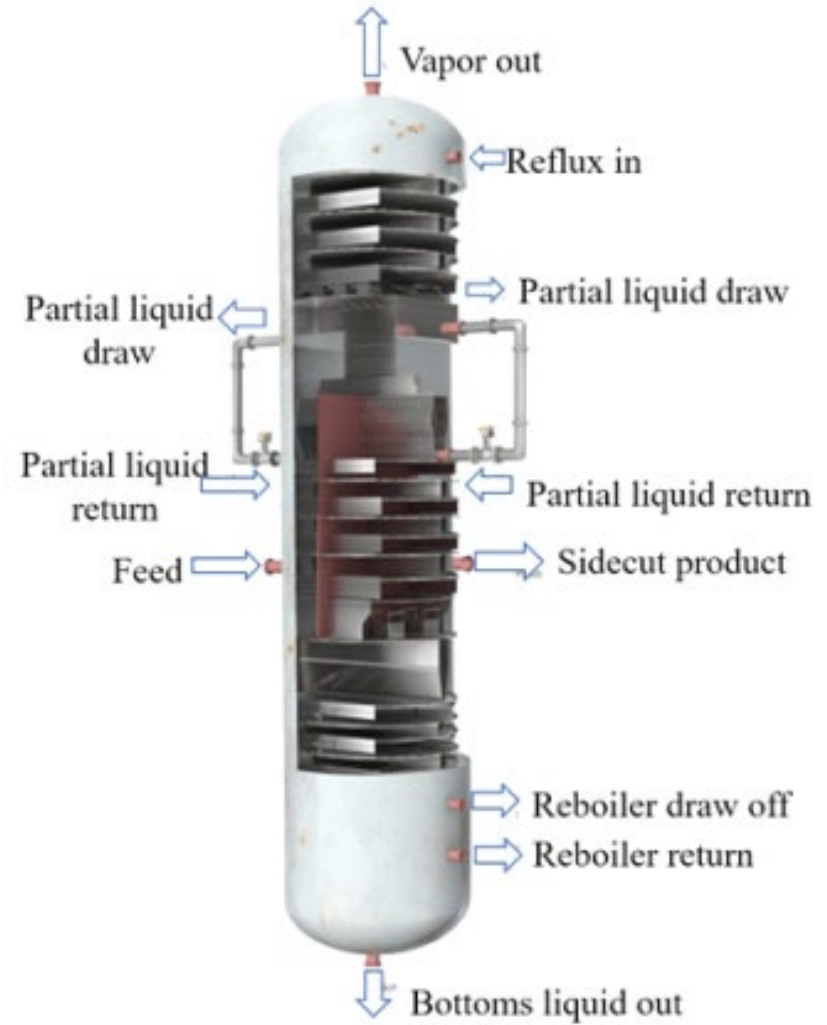
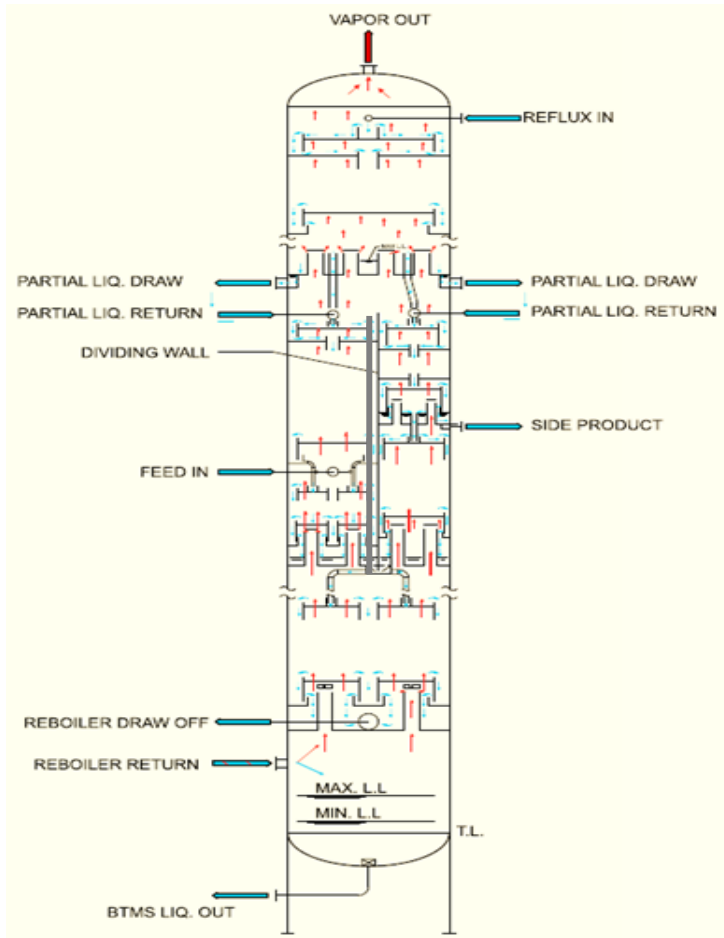


Thermally Intensified Distillation

- Thermally Coupled Distillation (TCD) and Dividing Wall Column (DWC)

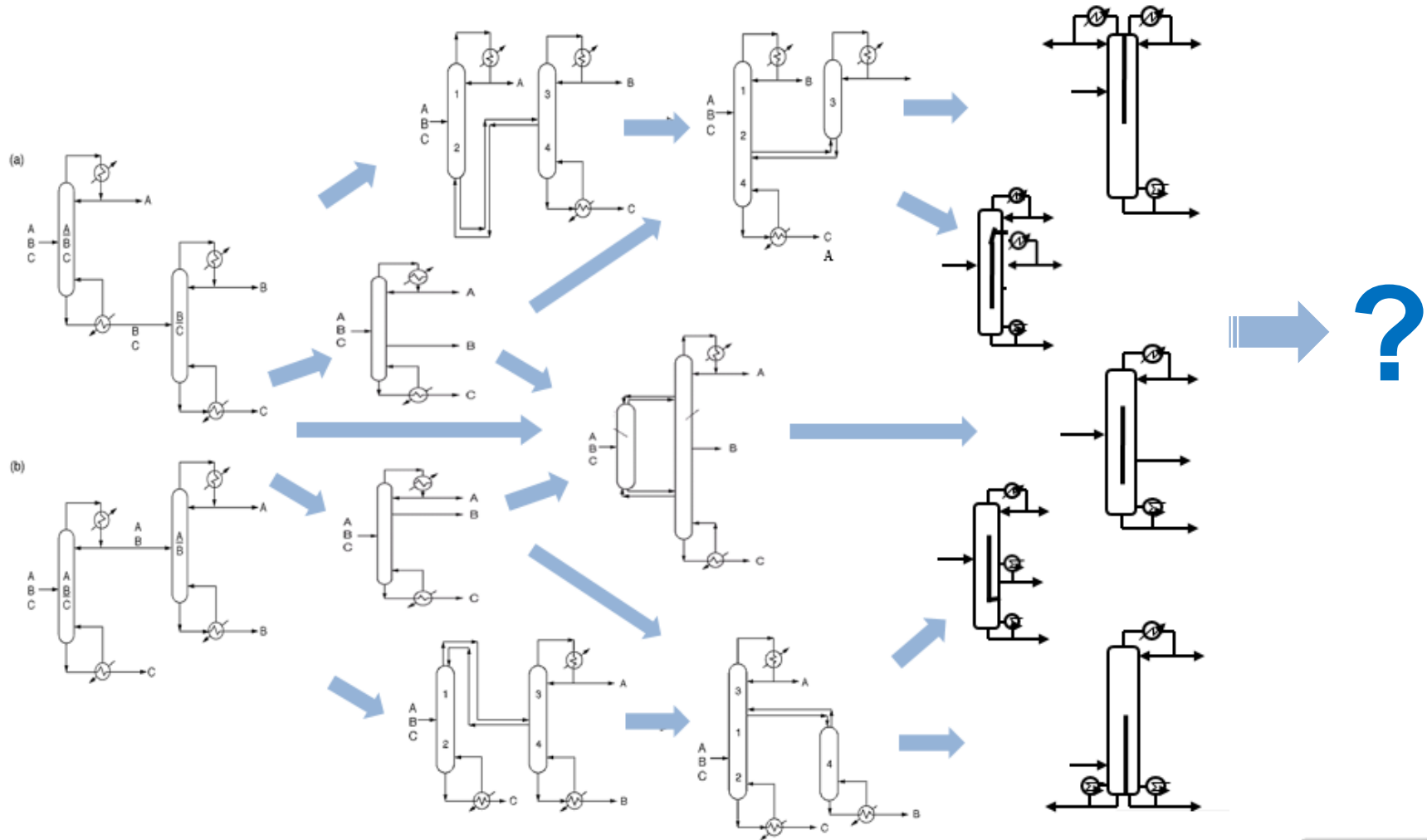


Dividing Wall Column as a fully intensified TCD



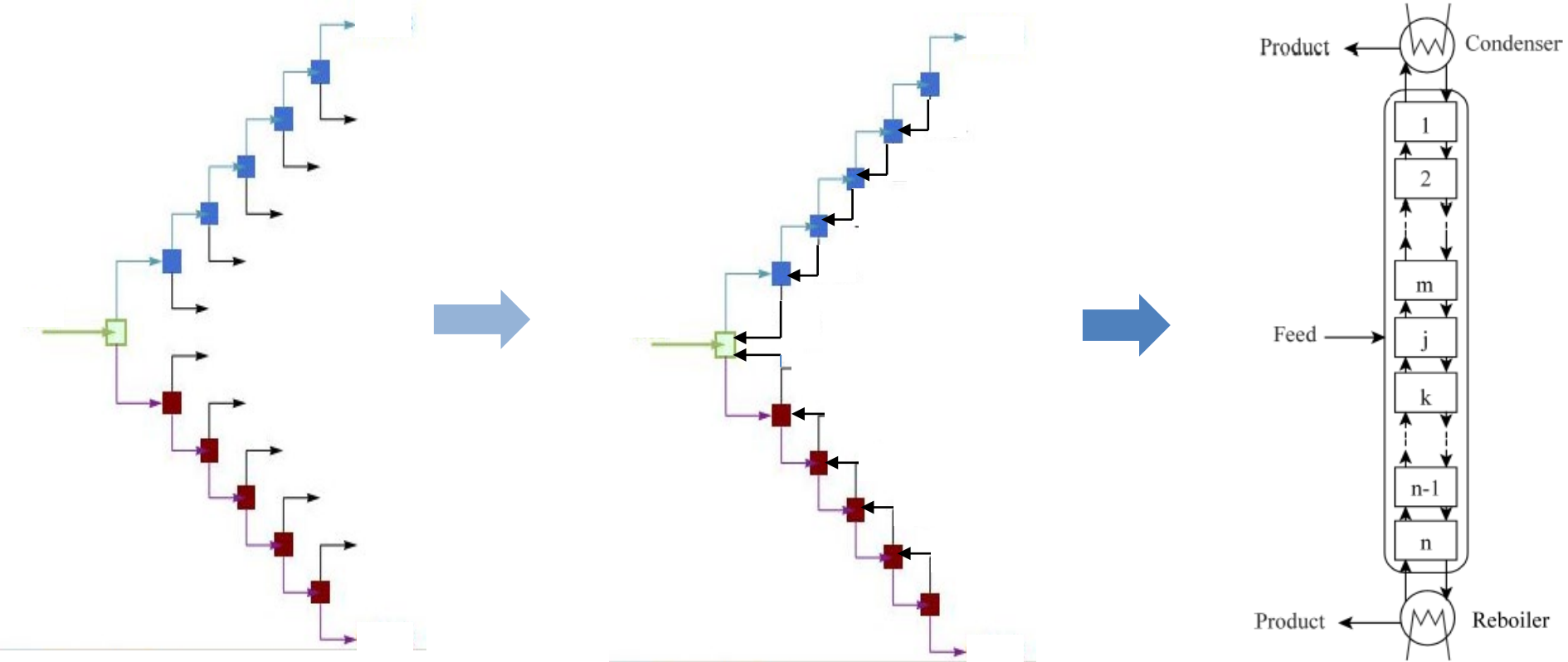
Thermally Intensified Distillation

- Evolution tracks from conventional ones to DWCs through TCDs



Conventional Distillation Column as a TCD

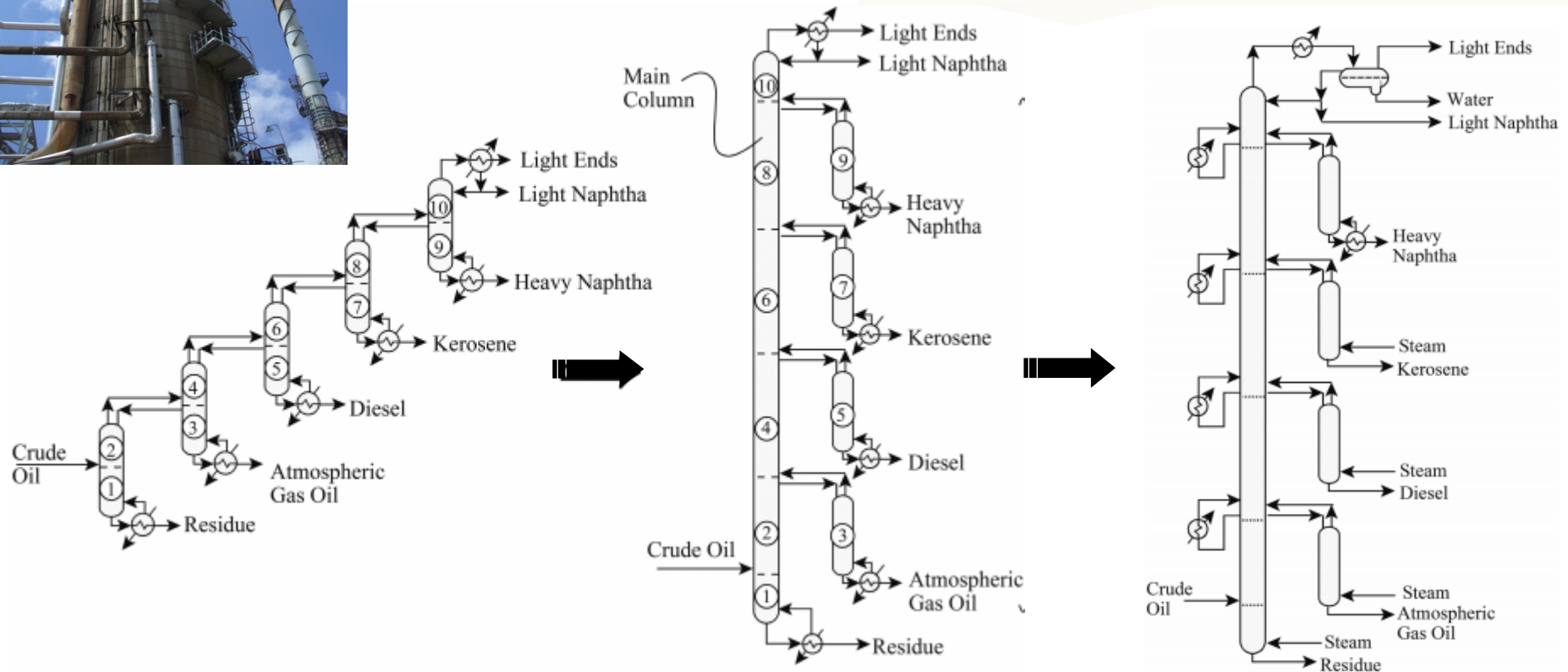
as an original TCD through vertical intensification of a multi-stage counter-flow flash drum process



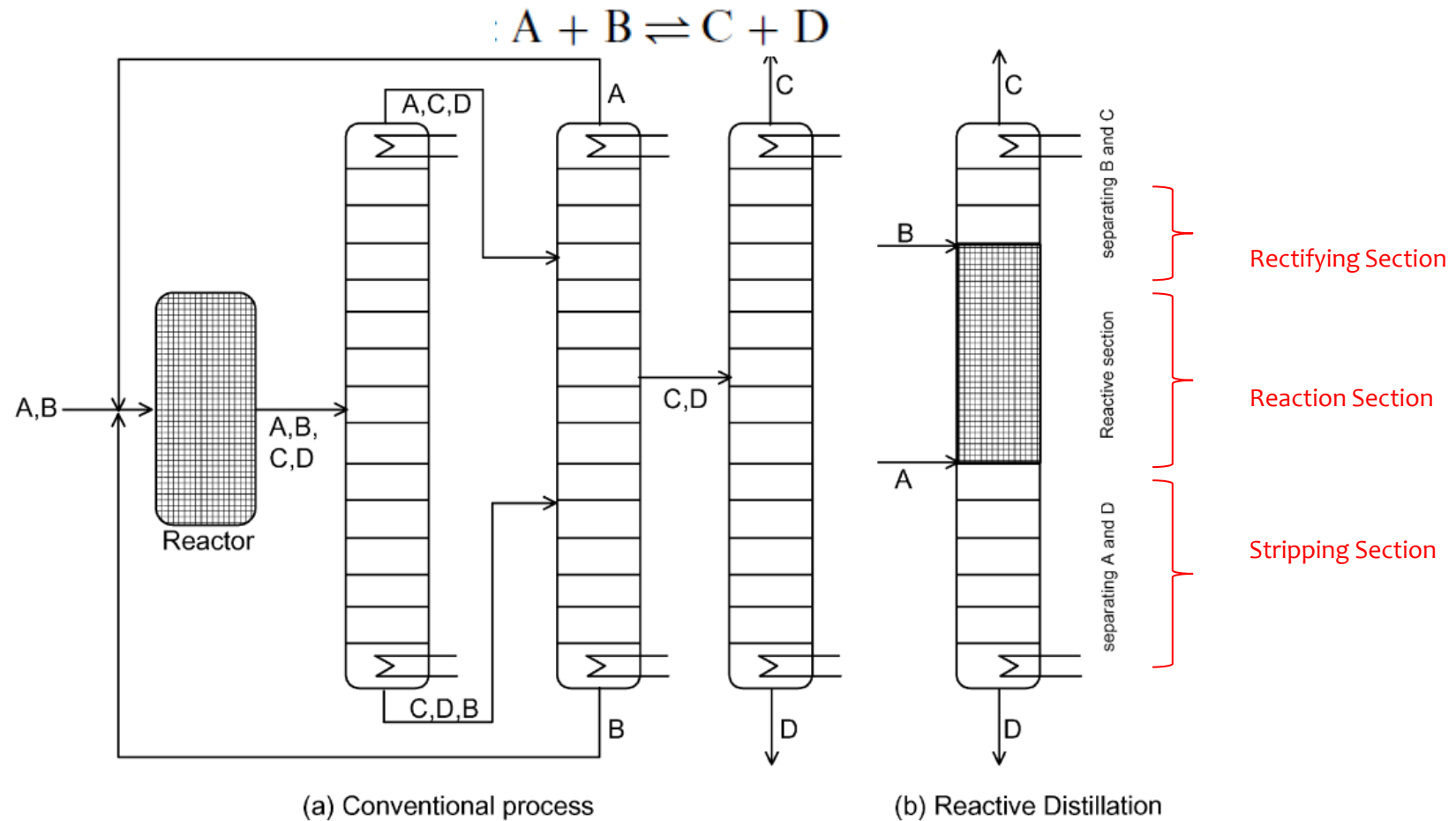
A- Tower as a more complicate TCD



- avoid high temp reboiling & fouling
- lowers partial P of comp & more volatile
- avoid huge vapor rise up



Reactive Distillation – Intensification of Reaction and Distillation

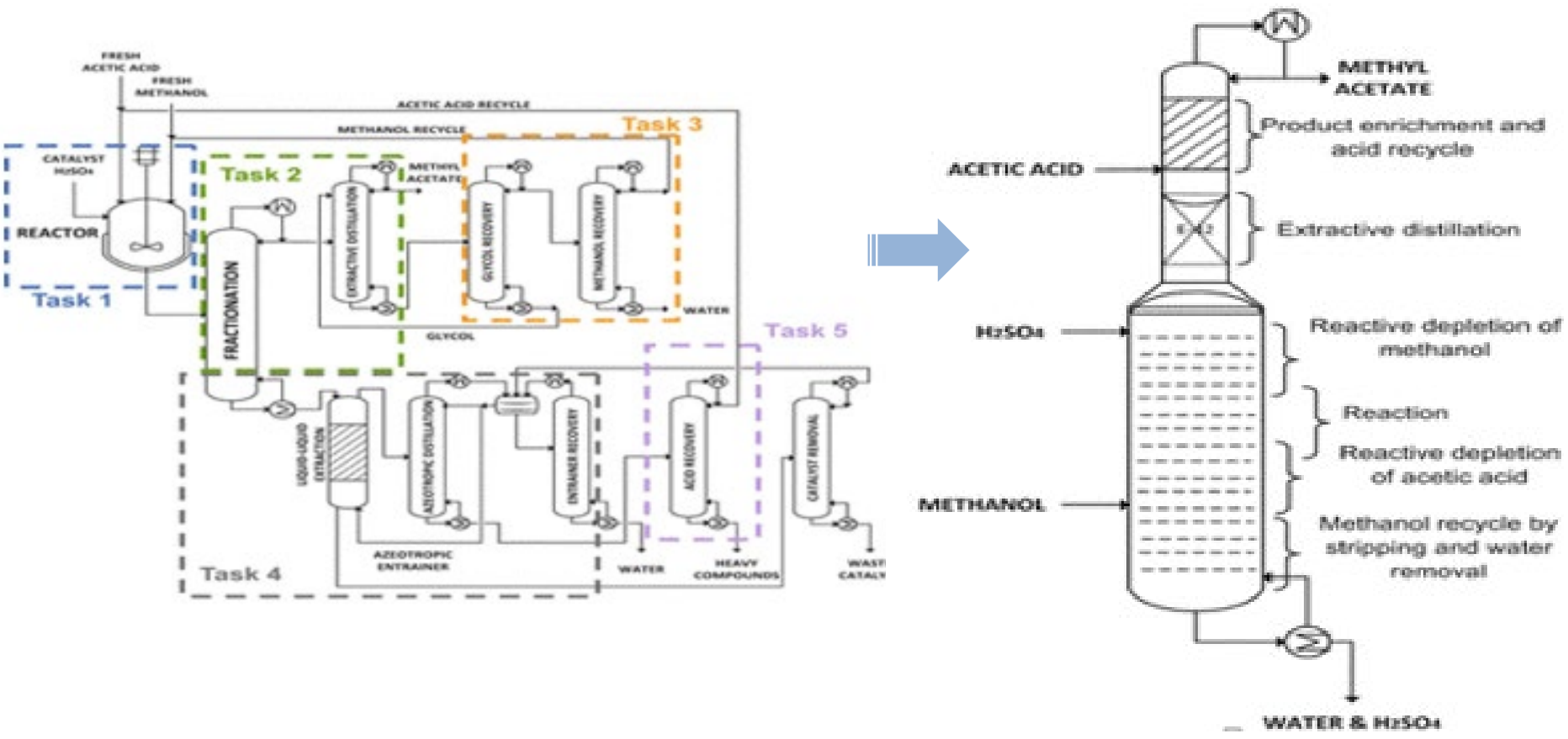


* Modelling reactive distillation R. Taylor!,", R. Krishna#

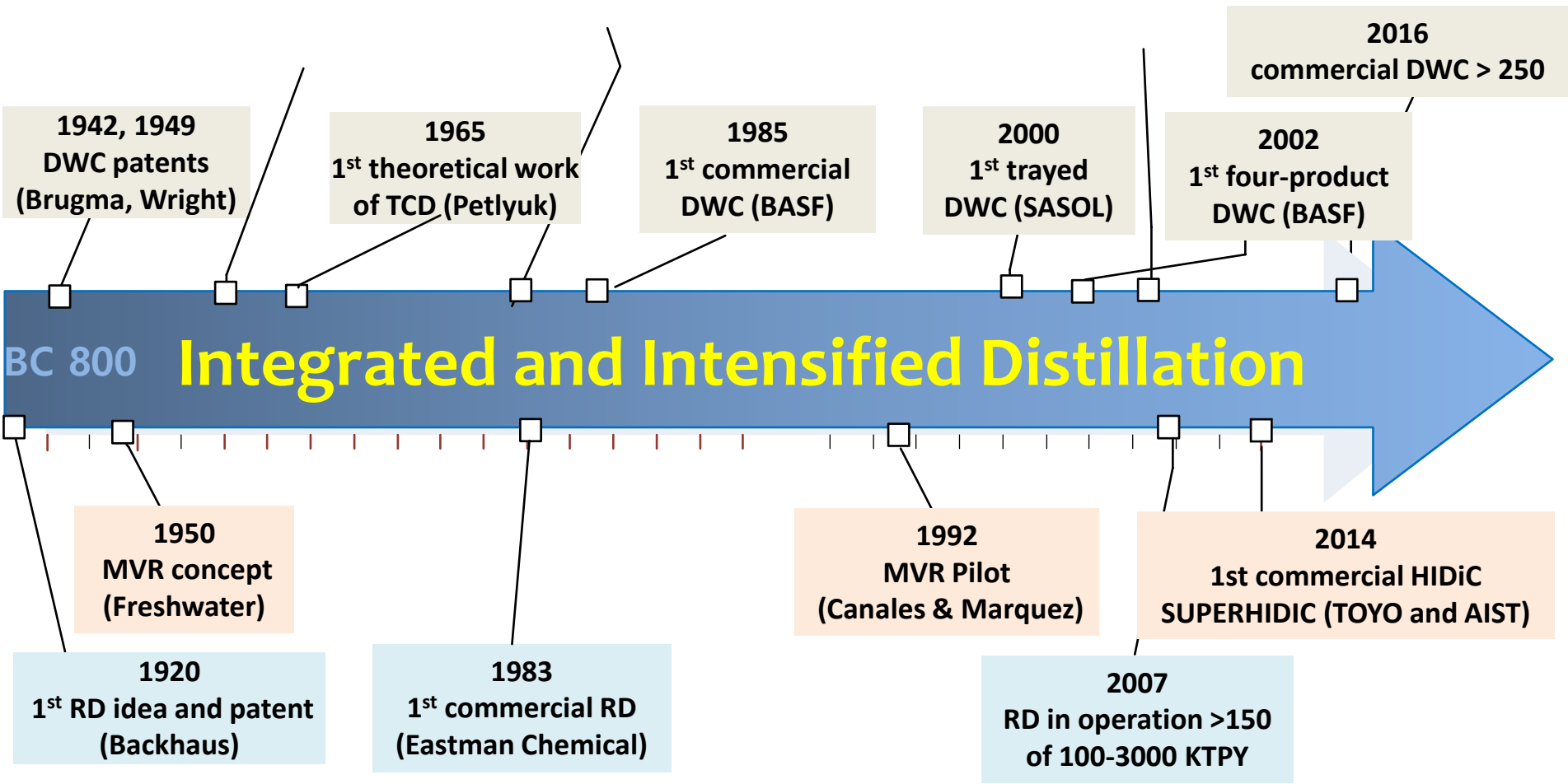
- Combining Reaction and Separation in a single vessel is termed as Reactive Separation Process.
- Significant Importance over Conventional Reactor-Separation Unit.
- Reduction in both energy and equipment costs.
- A single reactive column could be replaced a conventional multi-unit process that consumed 5 times more energy and capital investment

Reactive Distillation – Intensification of Reaction and Distillation

❖ Eastman Chemical Plant with 23 ton/hr commercial RD unit for esterification for methyl acetate production in 1983.



Integrated and Intensified Distillation – Yesterday and Today

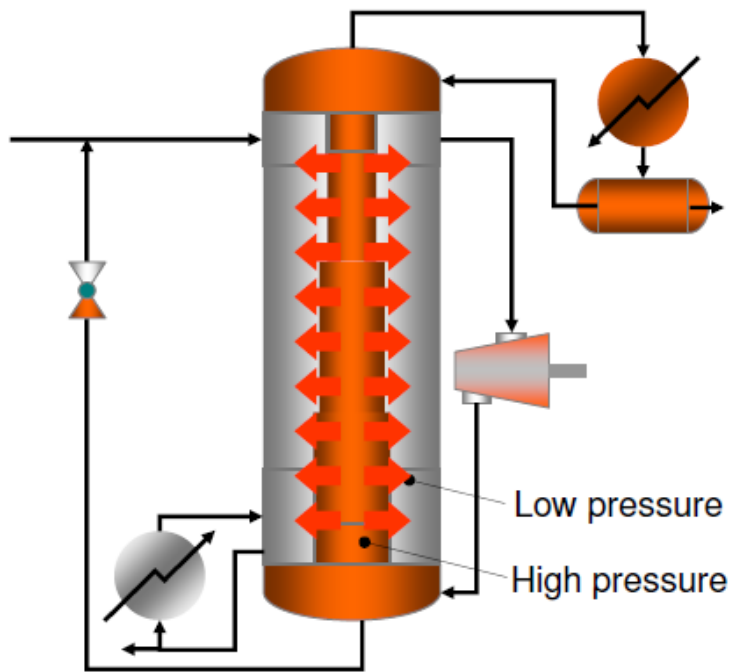


What it will look like?

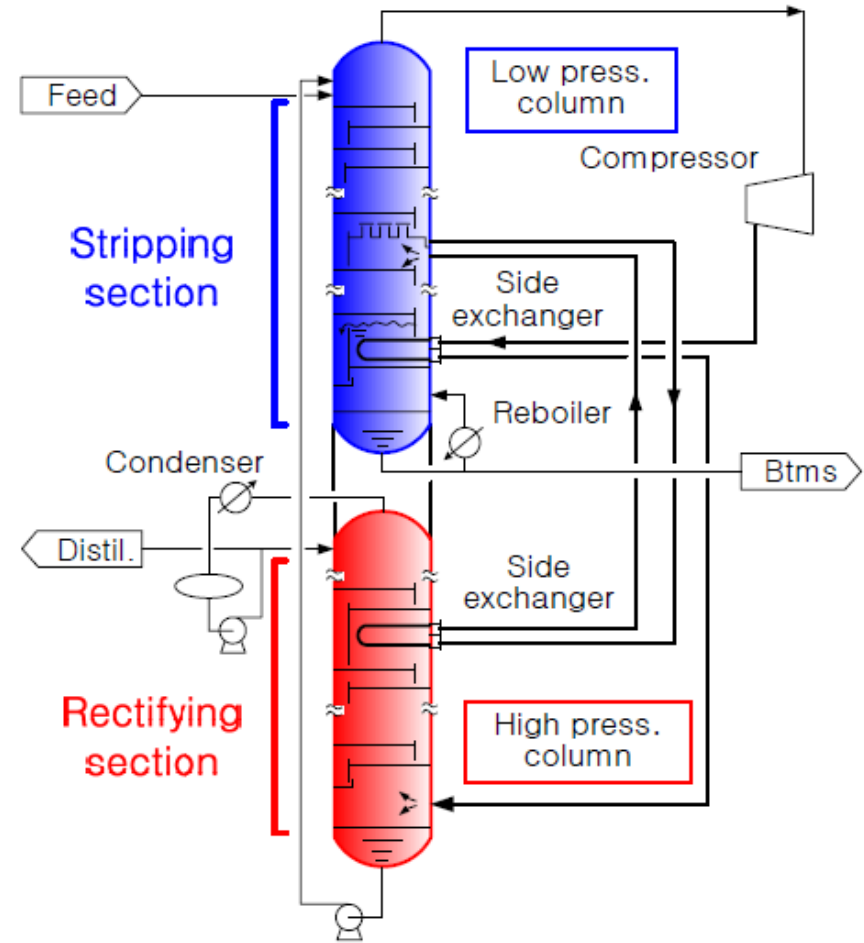
- It will come true in a practical alternative form.
- It will be more popular by overcoming main huddles and concerns.
- It will become more integrated, intensified, and combined.

Implementing Dreams via. Practical Alternatives

- It will come true in a practical alternative form !



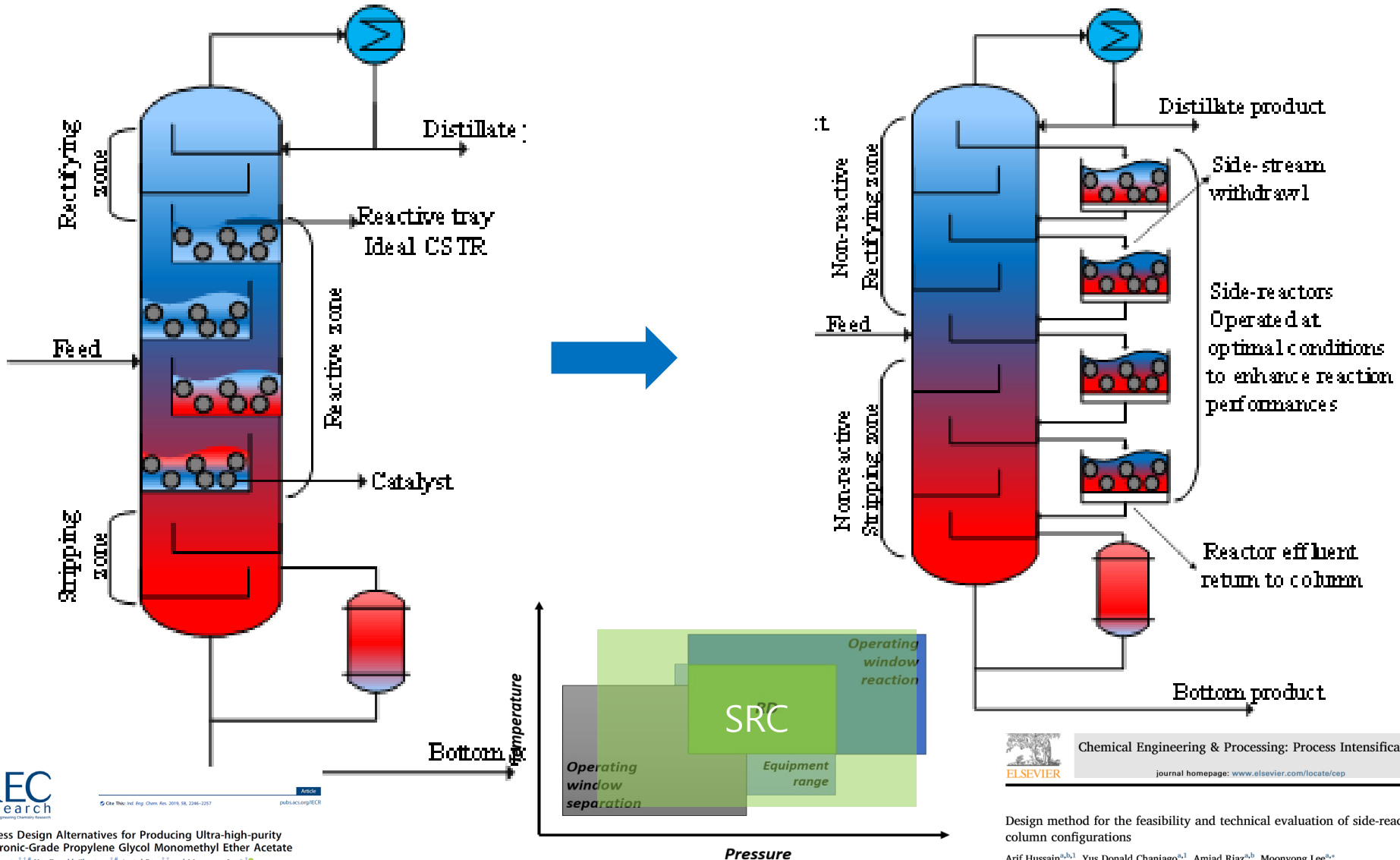
HIDiC



SuperHIDiC (TOYO and AIST)

Implementing Dreams via. Practical Alternatives

- It will come true in a practical alternative form !



Going over hurdles with innovative key unit technology

- more popular by overcoming main huddles and concerns !



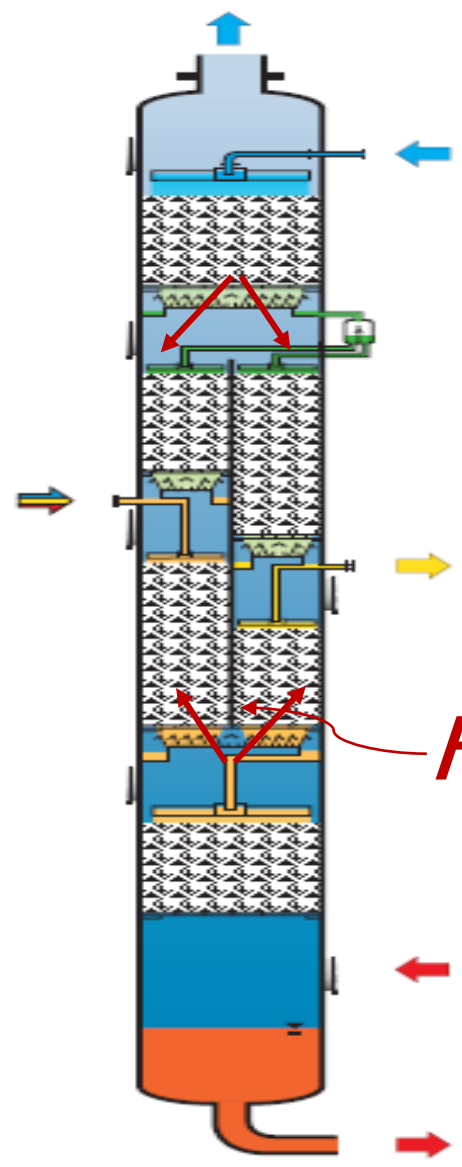
Hydraulic Driven Active Vapor Distributor for Enhancing Operability of a Dividing Wall Column



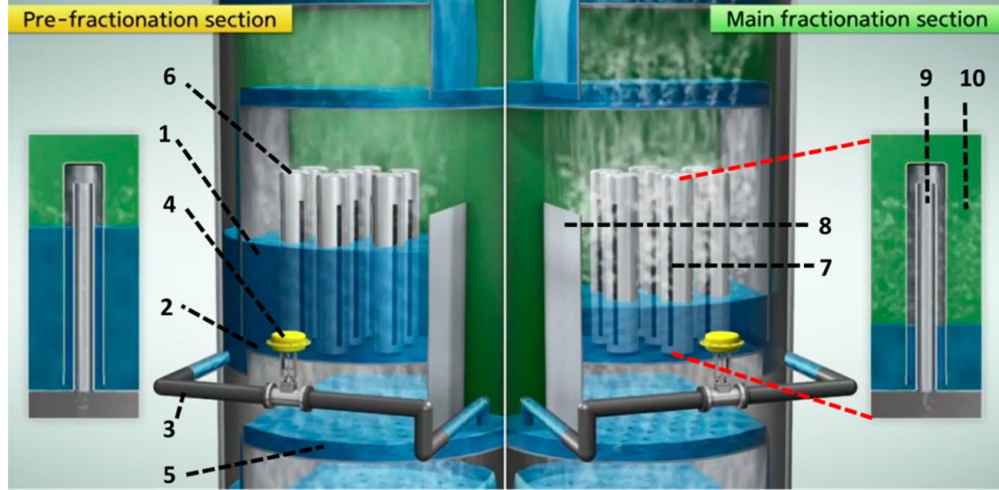
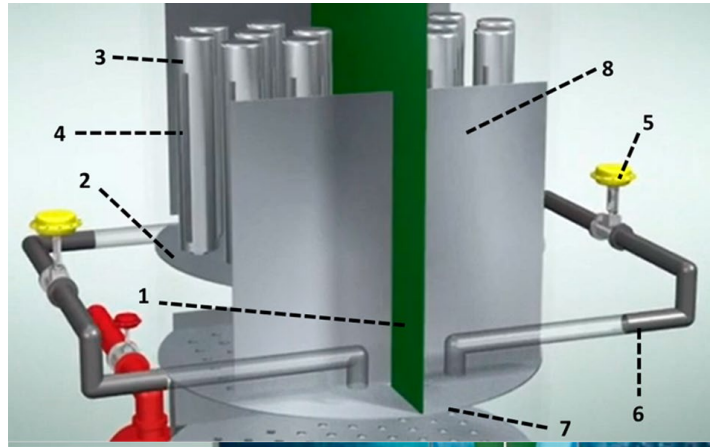
Chemical Engineering Research and Design
journal homepage: www.elsevier.com/locate/cherd

Optimal operation of a dividing wall column using an enhanced active vapor distributor

Gregorius Rionugroho Harvianto^a, Kwang Hyun Kim^a, Ki Joon Kang^{a,*,**}, Moonyong Lee^{b,*}

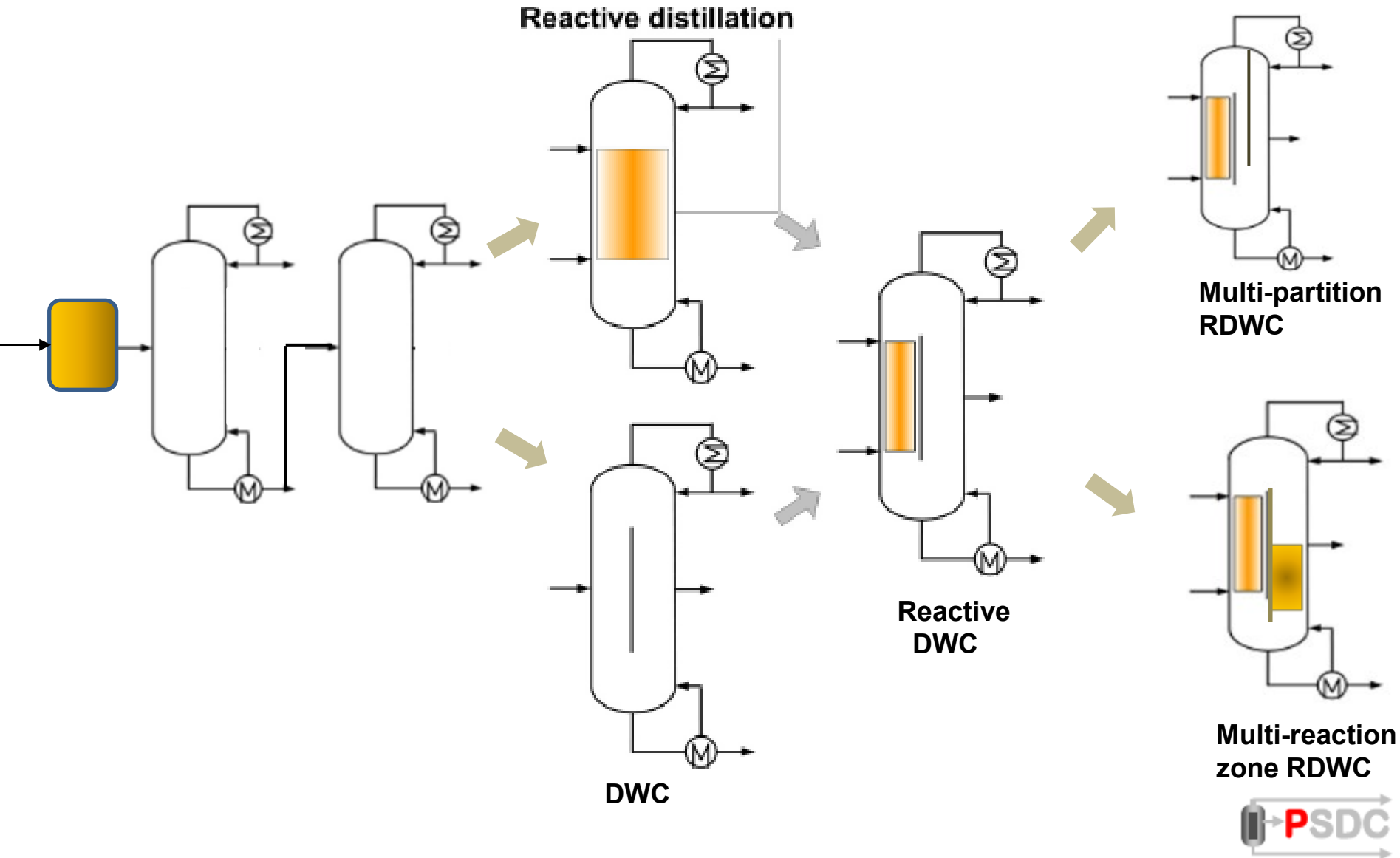


HOW ?



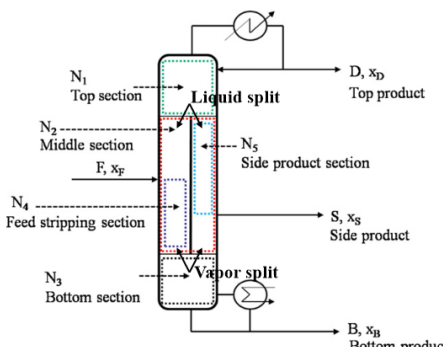
More Integrated, Intensified, and Combined

- more integrated, intensified, and combined



More Integrated, Intensified, and Combined

← Enhanced Optimization and UQ/UA by AI and Digitalization Technologies



$$Y = \beta_0 + \sum_{i=1}^k \beta_i X_i + \sum_{i=1}^k \beta_{ii} X_i^2 + \sum_{i < j} \beta_{ij} X_i X_j + \epsilon$$

where Y is the predicted response (total annual cost saving), X_i are the uncoded or coded values of the variables, β_0 is a constant, β_i , β_{ii} and β_{ij} are the coefficients of the linear, quadratic and interactive terms, respectively, and ϵ is the error term. MINITAB software was used for response surfaces fitting and optimizing the total annual cost saving.

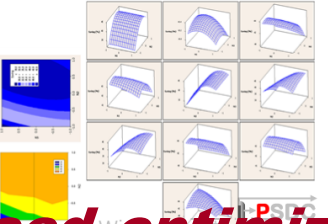


Dividing wall column structure design using response surface methodology
 Nguyen Van Duc Long, Moonyong Lee*
 School of Chemical Engineering, Yonsei University, Seongnam, 150-749, South Korea
 *Corresponding Author: E-mail: moonyong@yonsei.ac.kr
 DOI: 10.1016/j.ces.2018.04.021
 RAINBOW COMMUNICATIONS

Design and optimization of a dividing wall column by factorial design

Nguyen Van Duc Long and Moonyong Lee*
 School of Chemical Engineering, Yonsei University, Seongnam, 150-749, Korea
 (Received 1 August 2017 • accepted 23 August 2017)

Optimal	High	Low	RI	RI	RI	RI	RI
0.99739	0.99739	1.0	(0.13767)	(0.13768)	(0.13664)	(0.13769)	(0.13764)
			-1.0	-1.0	-1.0	-1.0	-1.0



Commercial Simulator Based Rigorous Model for DWC and TCD

Optimization Algorithm Library
 - Modified Coordinate Descent Algorithm
 - Particle Swarm Paradigm

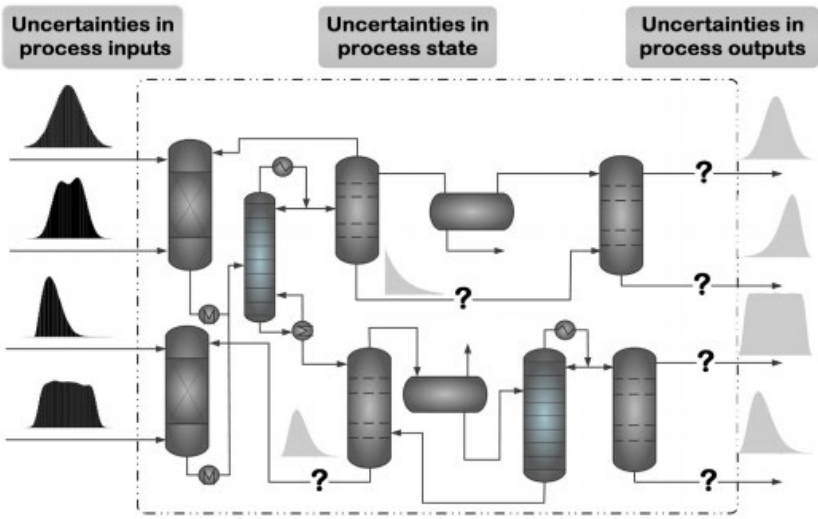
Main Features :

- Maintain solution rigor
- External optimizer embedded
- Expandable to other processes
- Utilize proven algorithms
- Choose interface languages

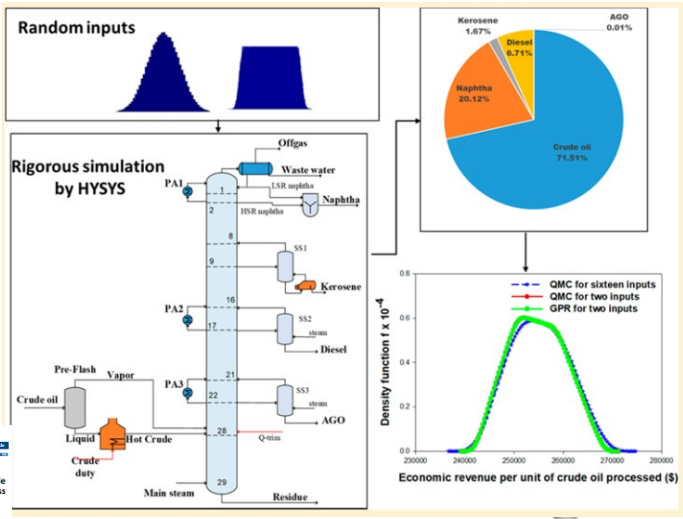
Embedded Visual Basic Code

Output Report

Enhanced optimization and control will become more important and essential!

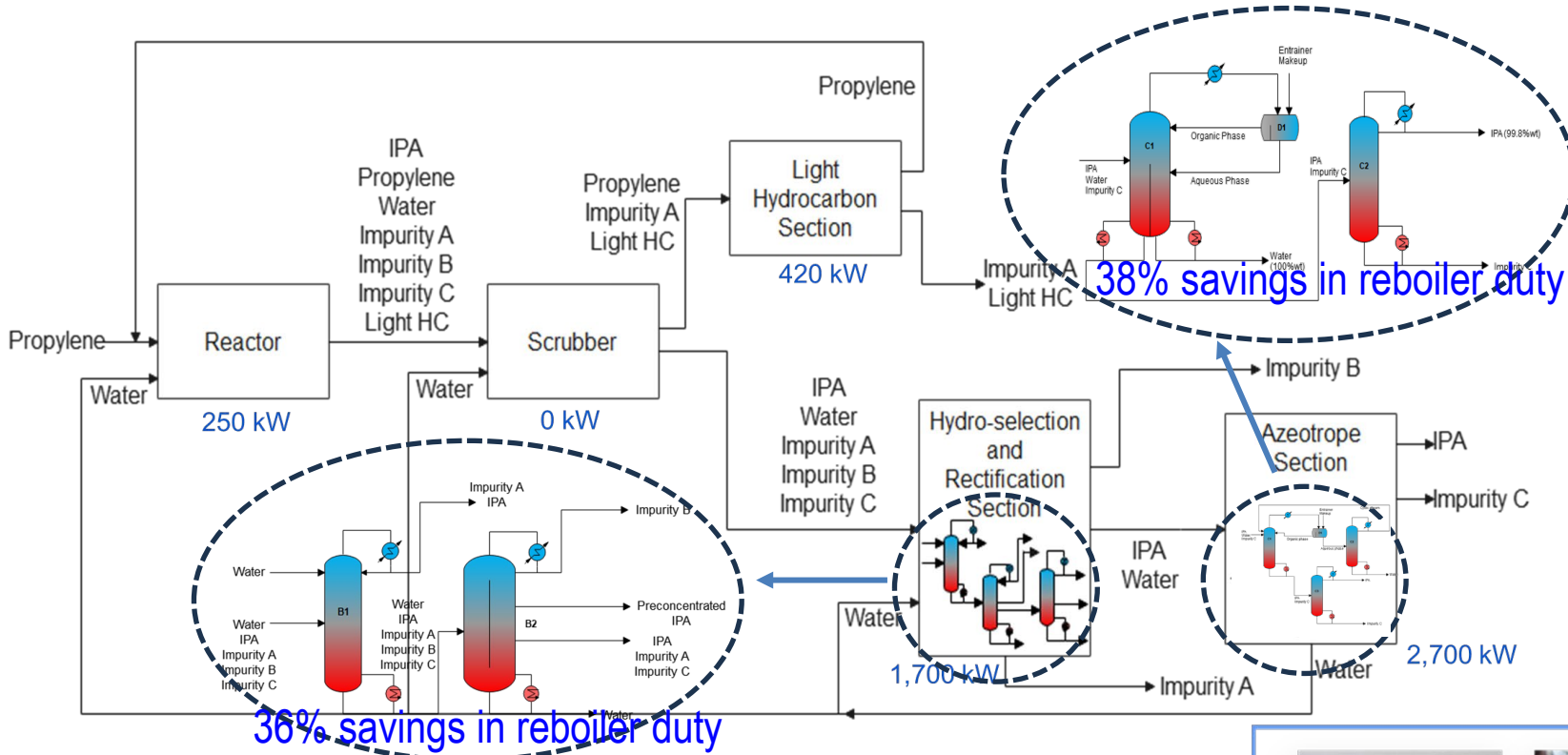


I&EC research
 Global Sensitivity Analysis and Uncertainty Quantification of Crude Distillation Unit Using Surrogate Model Based on Gaussian Process Regression
 Le Quang Minh*, Pham Van Trung Chung*, and Moonyong Lee**



IPA Production Process

- Heat Integration via. Process Intensification



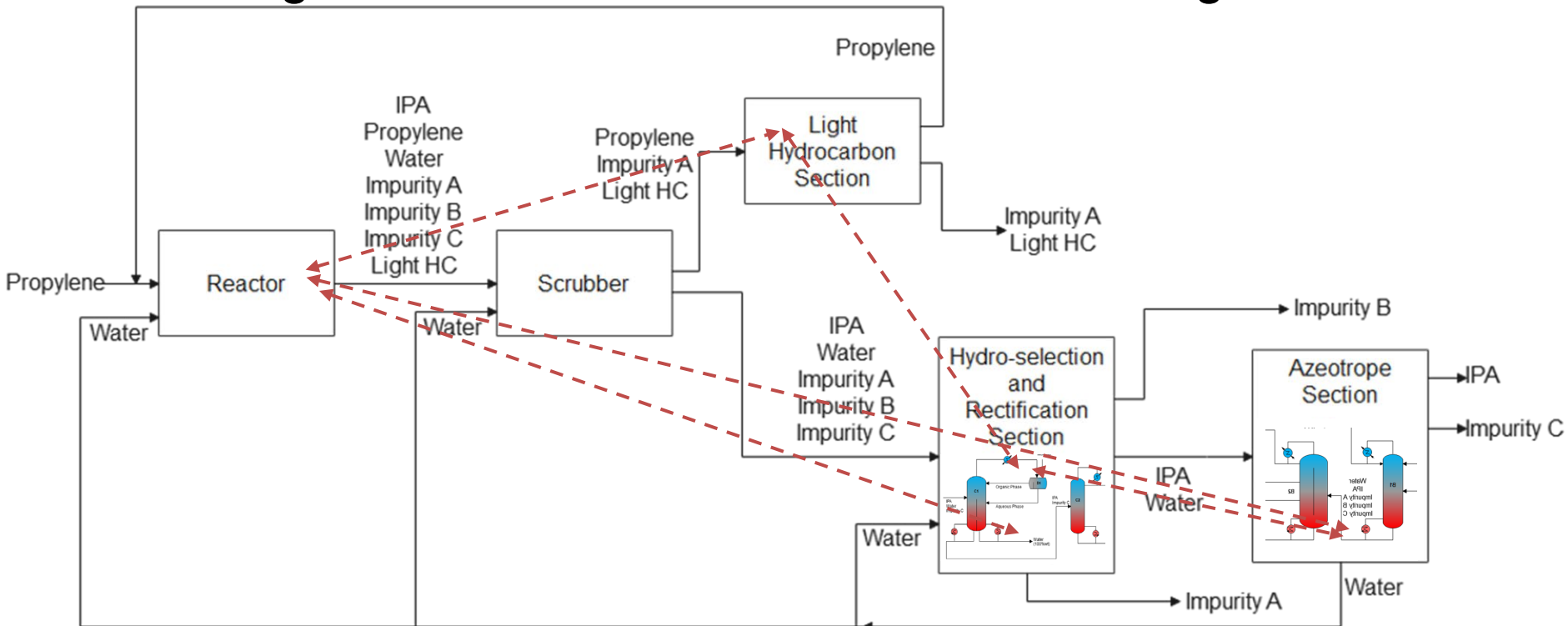
Total reboiler duty 4980 (kW) → 2980 (2087) (kW)



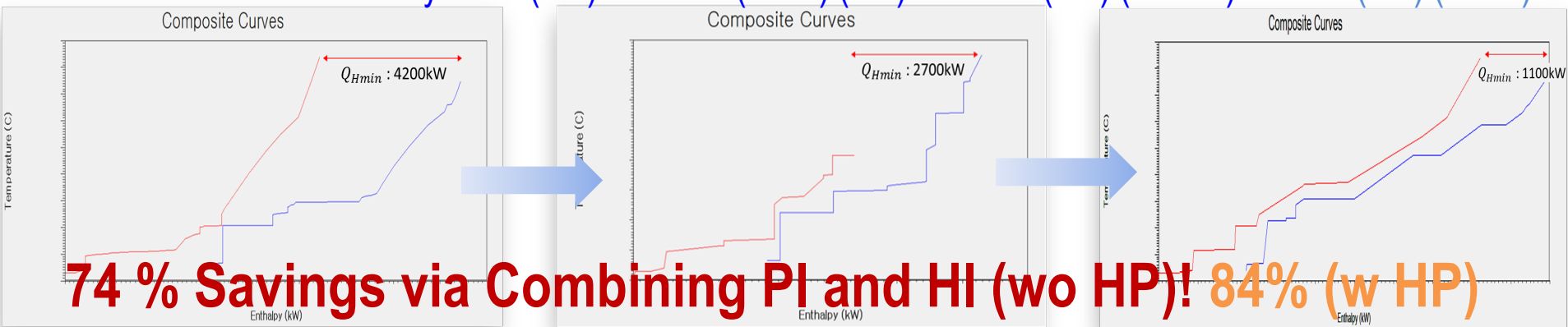
38 (57) % Savings via Distillation Intensification (with simple HI)!

IPA Production Process

- Combining Process Intensification and Heat Integration



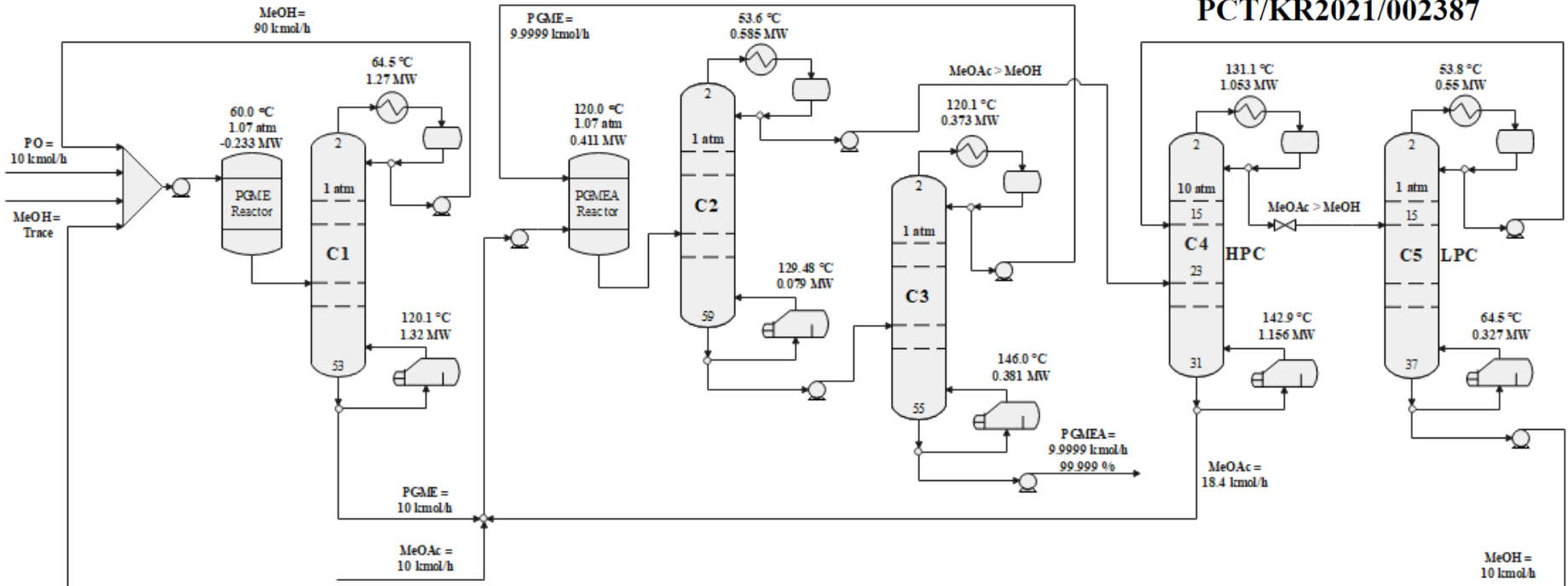
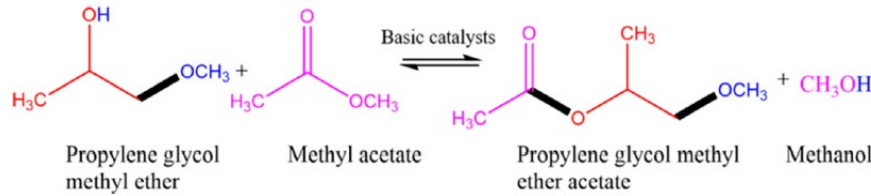
Total reboiler duty 4980 (kW) → 2980 (2087) (kW) → 1194 (kW) (wo HP) → 787 (kW) (w HP)



74 % Savings via Combining PI and HI (wo HP)! 84% (w HP)

PGMEA Production Process

Reactive Pressure Swing DWC Process for PGMEA Production



Reactive Pressure-Swing Distillation toward Sustainable Process of Novel Continuous Ultra-High-Purity Electronic-Grade Propylene Glycol Monomethyl Ether Acetate Manufacture

Yus Donald Chaniago,^{1,†} Anif Hussain,^{1,2,†} Rizqa Andika,³ and Moonyong Lee^{4,*}

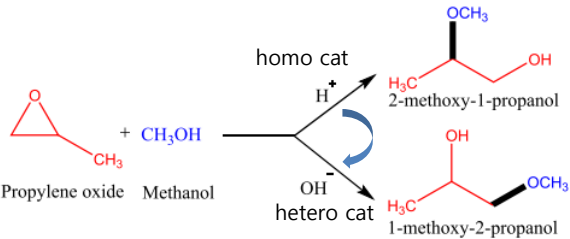
energies

MDP

Article
Pressure Swing-Based Reactive Distillation and Dividing Wall Column for Improving Manufacture of Propylene Glycol Monomethyl Ether Acetate

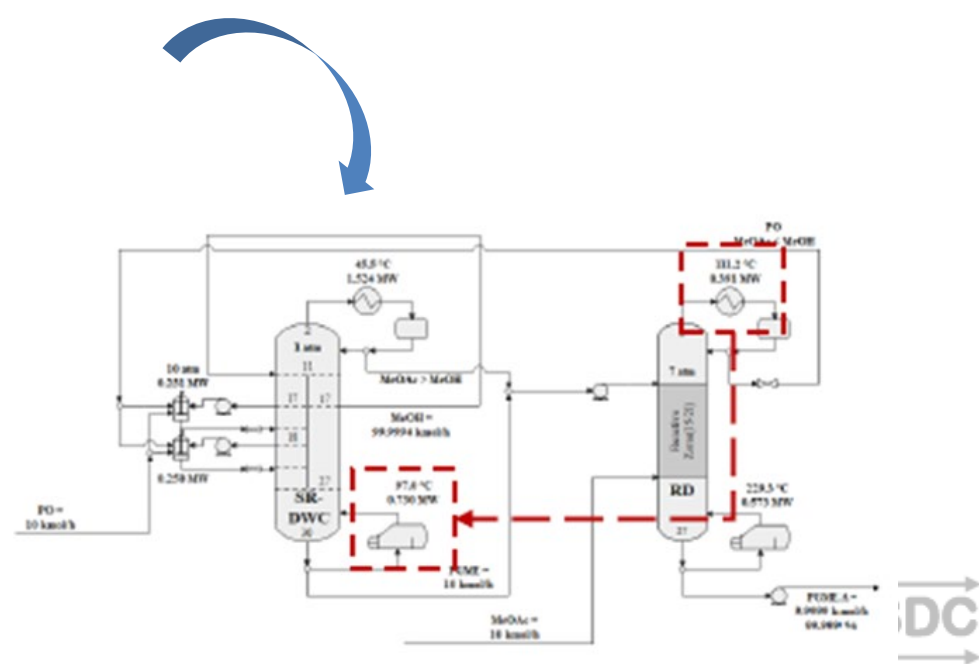
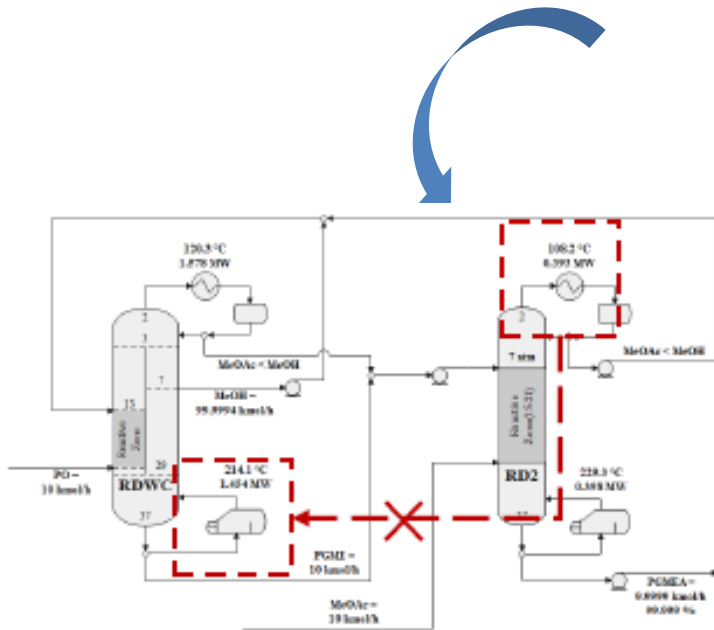
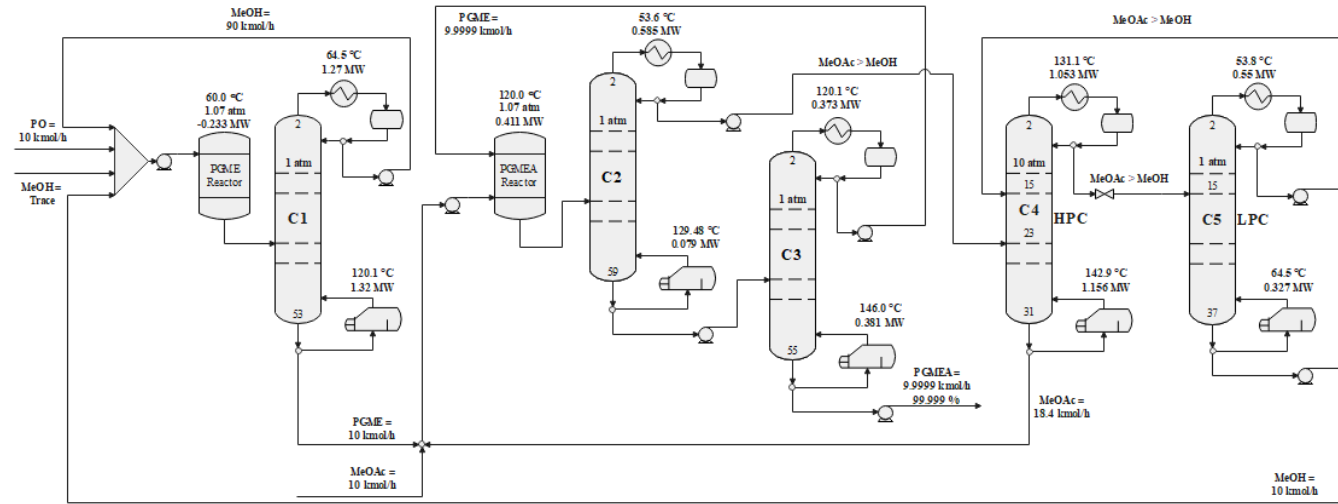
Yus Donald Chaniago^{1,†}, Le Cao Nhim^{2,†}, Ahmad Naquash³, Anjad Rizq³, Gwang Sik Kim⁴, Hanhwan Lim^{3,5} and Moonyong Lee^{4,*}

PCT/KR2021/002387



PGMEA Production Process

Reactive Pressure Swing DWC Process for PGMEA Production



DC

Conclusions

- PI^2 will be much more popular by extending its application to a real industry and by coming to us as it will :
 - come true in a practical alternative form.
 - overcome main huddles and concerns.
 - become more integrated, intensified, and combined.
- PI^2 will thus be one of effective and powerful ways and workhorses for sustainable process industry.