EALGAVIN

Energy Savings for Process Heat Exchangers: Case Studies and Benefits

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The Problem

Process improvement projects based on energy savings alone fail to attract funding

Rate of return is too low

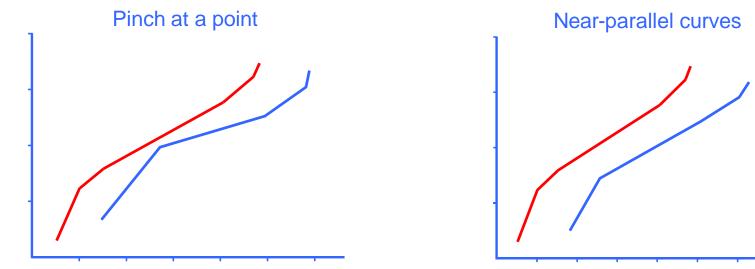
Reasons

- Traditional "pinch" analysis leads to increased plant complexity and requirements for new heat exchangers
- Plants without a well-defined pinch require modifications to a large fraction of the network to achieve savings
- New heat exchangers and modifications to pipework/structures are expensive





Composite Curves - Poorly Defined Pinch



A few plants have a clearly-defined pinch:

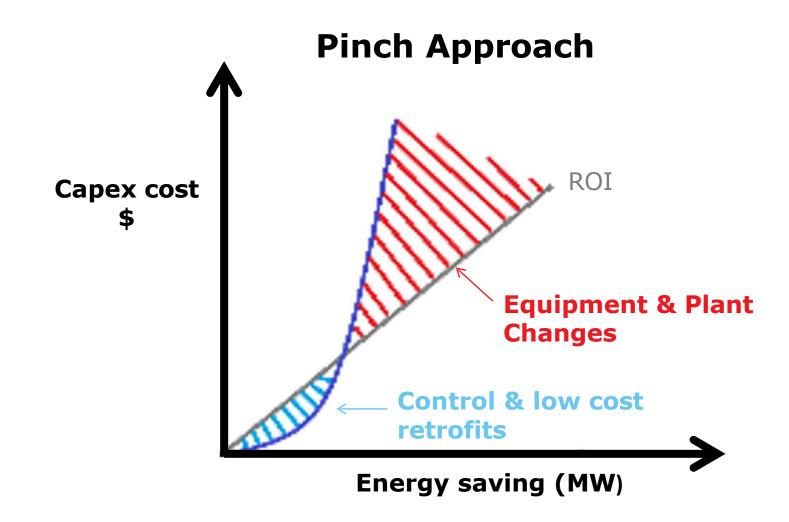
 Modest network modifications near pinch point will yield energy savings at low cost

For many plants composite curves are near-parallel:

 To achieve energy savings, modifications will be required across the majority of the network – high cost



Project Costs vs. Energy Savings



Solutions

Increase the energy savings

• Limited by thermodynamics

Reduce project cost

- Avoid structural changes to the network
- Avoid new equipment
- Improve performance of installed assets

Introduce other motivating factors

- Increased throughput
- Improved product quality
- More profitable product mix





Software and Analysis

Bring together two technologies

- Heat exchanger network
 simulation/optimisation
- Heat exchanger enhancement

Use specialist software to

- Identify opportunities to use enhancement
- Select the most appropriate enhancement technique
- Quantify the outcomes
- Demonstrate operational flexibility





Global Consulting Engineers for Heat Transfer Solutions

- CALGAVIN established 1980
- Head Office: Alcester, Birmingham, UK
- Manufacturing of technology carried
 out in UK

Extensive Research and Development in Hardware & Software

Work carried out at In-house Test Laboratory collaborating with 10+ Universities across Europe.





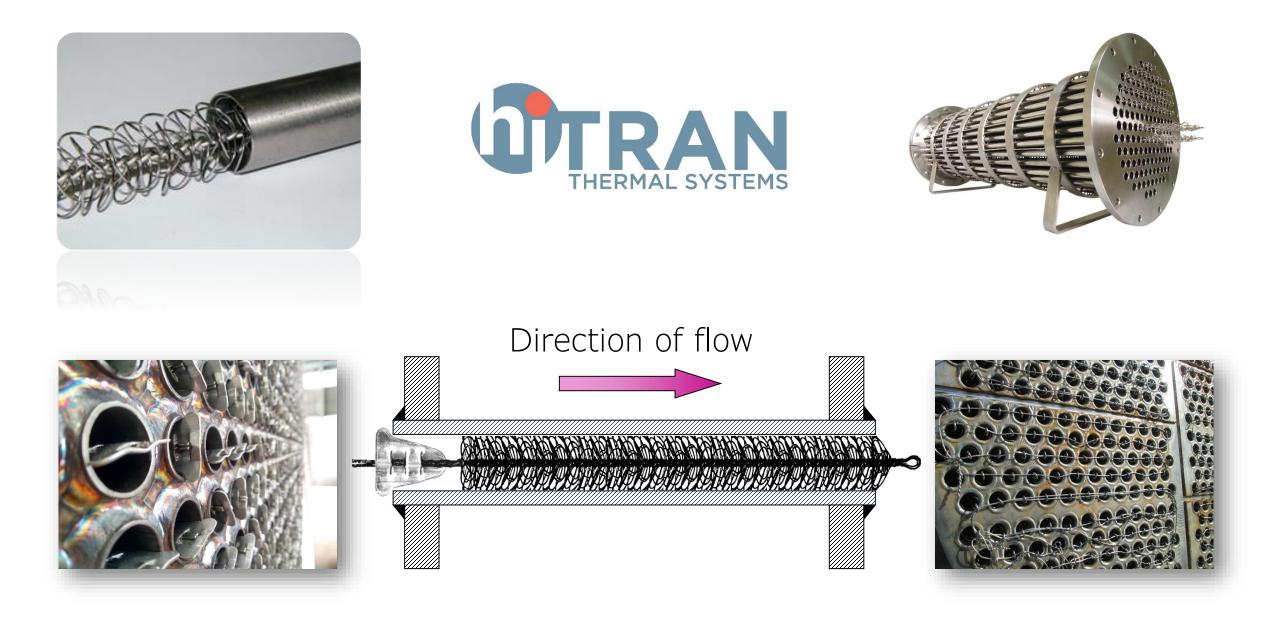
Engineering Services Provided

- Analytical engineering
 - Advise on design and performance improvement of new and existing heat exchangers
- Design services
 - Evaluating specifications and modelling thermal & hydraulic ratings (HTRI[®], Aspentech[®] EDR & CALGAVIN[®].SP)
- CFD analysis
 - Identify heat exchanger poor performance root caused by maldistribution, stratification or other causes via CFD



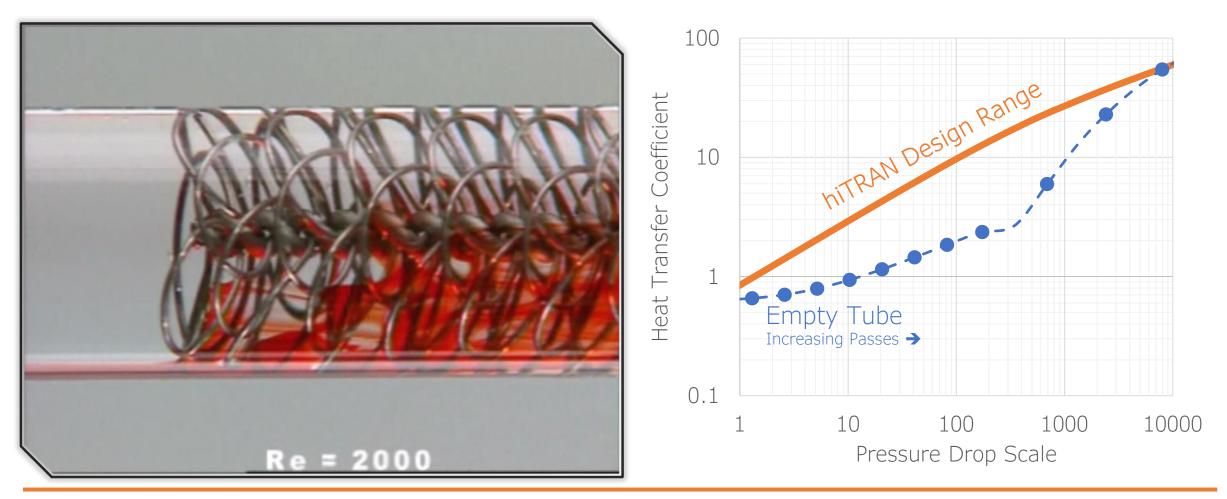






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Heat Transfer Enhancement



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CFD Simulation of Laminar Flow vs hiTRAN-Enhanced

77.0

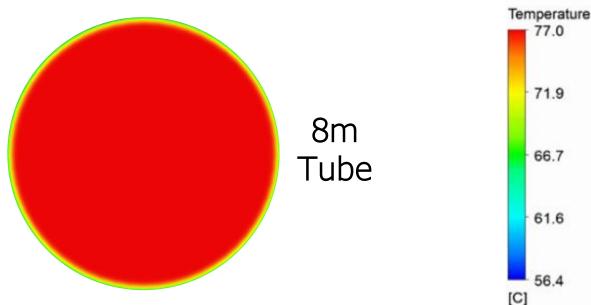
71.9

66.7

61.6

56.4

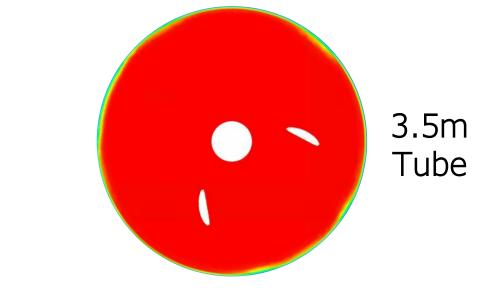
Plain Empty Tube Stratified flow Lower half of tube not effective



Natural convection:

Cold, heavy fluid sinks to the bottom of the tube

Enhancement with hiTRAN Tube Fully mixed flow Common temperature across tube



hiTRAN-enhanced flow delivers a • reduced flow length by 56%

Target Applications for hiTRAN® Technology

TOTAL Angola, Wet/Dry Crude Exchangers



PTT Thailand, Lean/Rich TEG Exchanger



SINOPEC China, EOG Condenser



LUKOIL

Russia, Feed Effluent Exchangers



ESSAR OIL UK, Diesel Rundown Cooler



BASF Germany, Thermosyphon Reboiler



DOW Chemicals Germany, Epoxy Resin Cooler



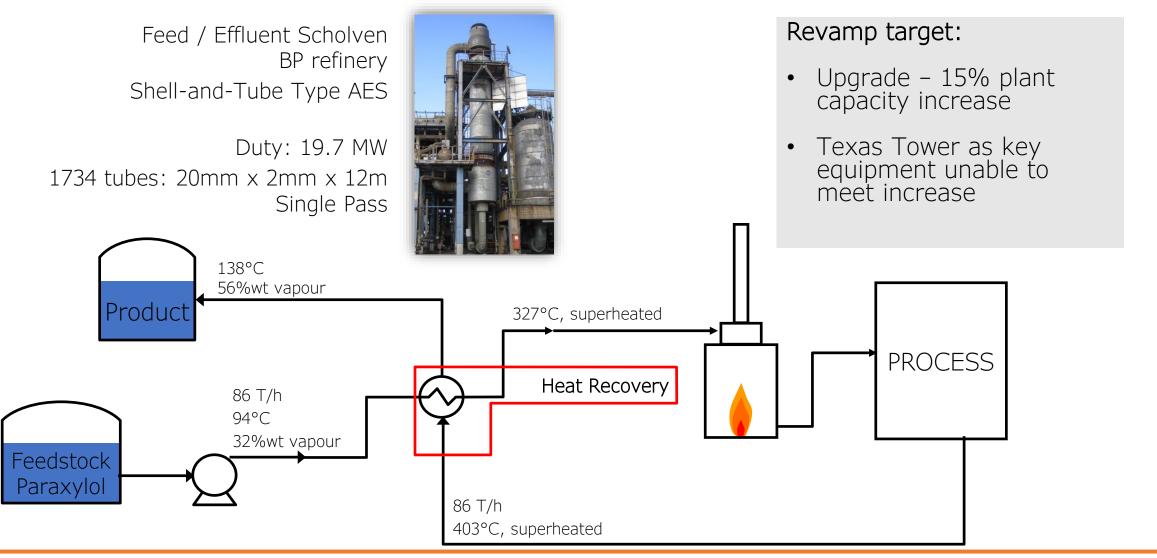
TOTAL Belgium, Ethane Vaporiser



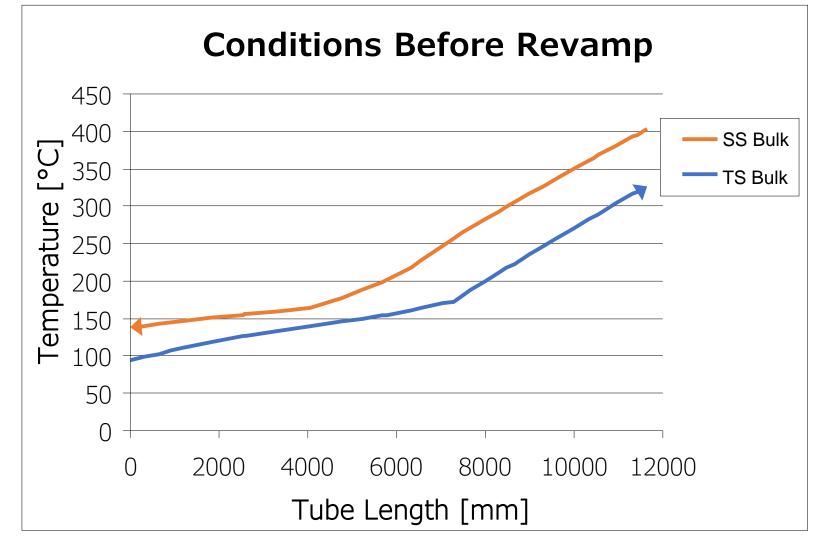
Case Studies Heat Recovery & Energy Savings



Heat Recovery - Feed / Effluent HEX



Temperature Distribution



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Problems with Current Design

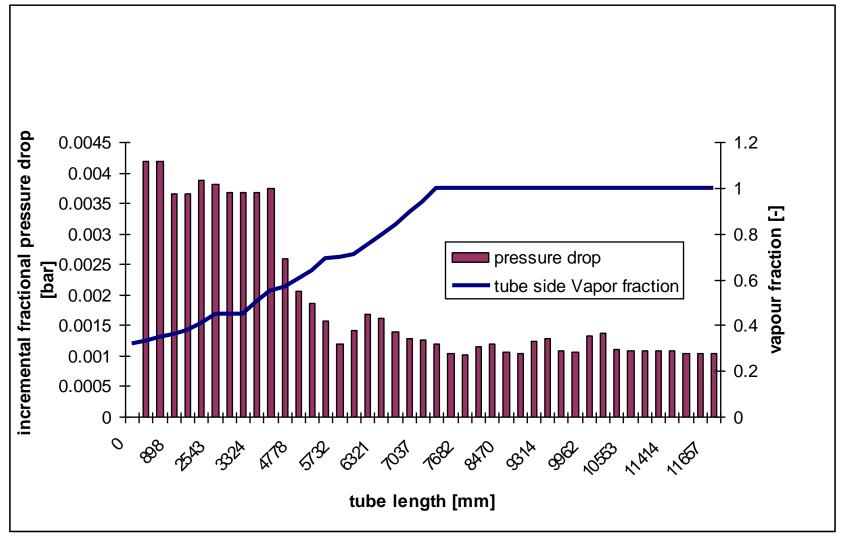
- Temperature cross; single tube pass only
- Low tube-side heat transfer
- 1 bar pressure drop allowable, only 0.1bar used

Options for Upgrades

Size Increase (New exchanger, incl. new piping & civil eng.)
 hiTRAN Enhancement technology

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Provided Solution



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The Benefits



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- 3MW increase in duty, 18% higher throughput
 - Negated need for larger unit, saving in CAPEX
 - No additional civil engineering costs
 - No additional piping costs

- Reduction in Fired Heater duty
 - Reduced energy use
 - Reduced CO₂ output (80,000 t since installation in 2008)
 - \$3.2 M savings since 2008 with a Carbon Credit price \$40/t

Feed/Effluent Exchanger Enhancement

Exchanger

- Heat recovery from reactor effluent
 - Additional pre-heating provided by fired heater
- TEMA AES, 3 series x 2 parallel shells
- 2,521 tubes per shell (9m long)

Problem

- Insufficient heat transfer for higher throughput
- High fuel consumption in furnace (at firing limit)

hiTRAN[®] Benefits

- Improved heat transfer performance
- Reduced maldistribution on tube-side
- Increased duty of 2.2 MW (+50%)
- Increase plant throughput
- Alternative: Fuel saving of \$233,000 per year







New Design: Export Oil Trim Cooler

End User

Kuwait Oil

Service

Export Oil Cooler Duty: 9.7MW

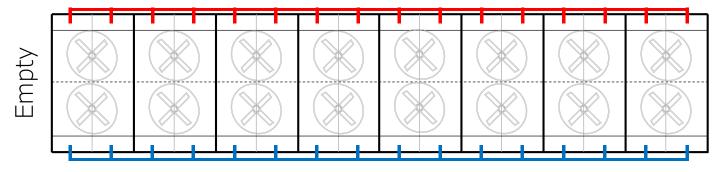
Oil Flow 125 kg/sec Inlet: 100°C Outlet: 60°C ΔP Allowed: 103.4kPa Air Cooler Duty - 9.7 MW

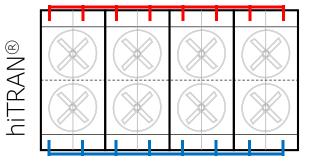
Exchanger API 661 Forced draft air cooler 8 Bays in parallel, 2 bundles per bay 600 tubes per bundle (31.75 x 2.1x 12,800mm)

Ambient Temperature: 50°C ΔP allowed: 200 Pa Face Velocity: 2.1 m/sec

Case Study: Export Oil Trim Cooler





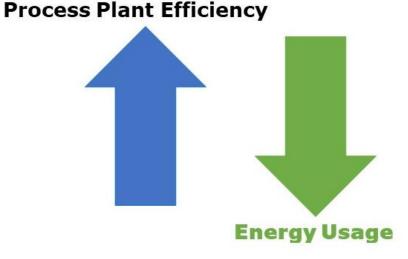


	Empty Tube Design	hiTRAN [®] Design
Heat Transfer Coefficient (W/m ² K)	50	252
Bays in parallel	8	4
No of rows / passes	12 / 8	11 / 2
Tube per bundle / Total	600 / 9600	473 / 3784
Plot area (m ²)	712.3	309.7
Fan Power (kW)	271	107
Predicted cost after 10 years	\$3,100,000	\$1,200,000 (incl. hiTRAN®)

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Cost and Energy Savings with Enhancement

- Good return on investment Increased heat transfer but at small CAPEX cost compared to the alternative of replacement plant and re-piping.
- Reduced OPEX costs Less cooling/heating utilities needed for required heat transfer duties.
- Increased productivity Increases the duty of an exchanger enabling increased flows to be processed and increase throughput.



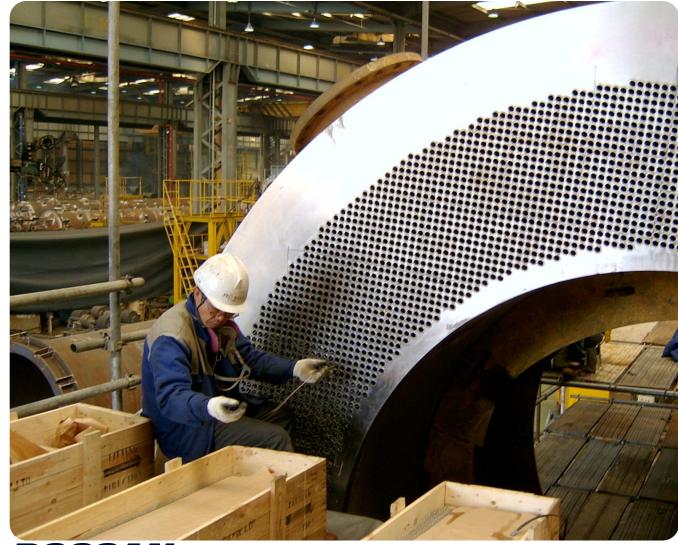


Completed Orders 20,000+

Successful Retrofits **5,800+**

Countries Supplied **50+**

Number of Industries **15+**

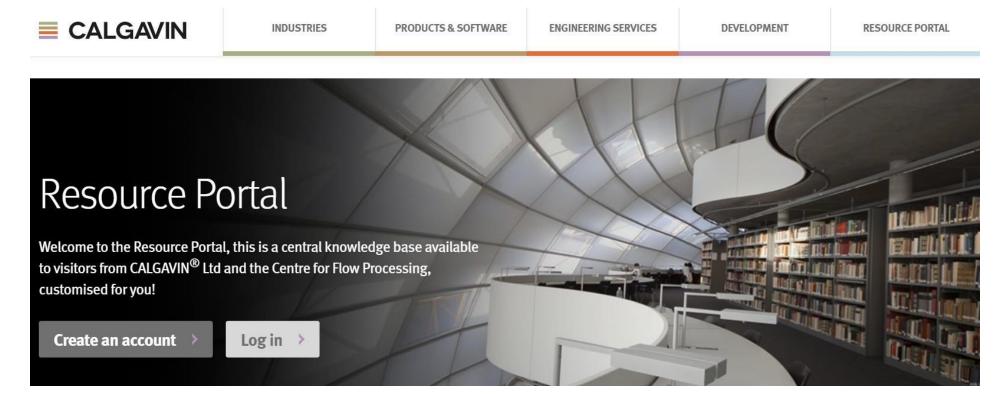






CALGAVIN Resource Portal

https://www.calgavin.com/resource-portal



CALGAVIN has a protected customer resource portal and knowledge base to explore and learn!

- Case studies (Offshore, Refining, Petrochemicals & Chemicals)
- Academic papers, conference papers & magazine articles
- Over 20 webinars (Heat exchanger design, condensation, maldistribution, vaporisation etc.)

Any questions?



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