

Best Practice: Digitalisation of Operational Safety for O&M Practical Strategy

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Contents



Challenges | The Case for Change

Peeling the Layers for Process Safety

Application of the Right Tools | AMS, IPL, Boundary & CLPM

Digitalisation & Centralisation | Used Case Adaptation

Value Creation | Policing to Consulting

Case for Change | Operations Value Leakage from Data Searching



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"Engineers typically spend 30% of their time looking for information. A digital thread provides a means to significantly reduce this value leakage." - ARC Advisory Group, 2021 –

Our customers locate data & document 30 – 50% faster with 50% travelling time reduced for verification at site



Case for Change | Challenges of Performance Monitoring



Manual Intervention

80% time spent on data extraction & reporting – leading to human error

Localised Data

Data resides in local machine and is unavailable online for interaction with other digital solutions

Reactive

No early warning indications on equipment performance & deterioration





Automated Updates

Automated data retrieval and report generation with virtual analyser functionality

Data Centralisation

Online server with hourly data generation, ready for integration with any digital application

Predictive

Visualizing integrity & performance of instrumentation and control system to make more informative decisions

Conservative Approach

Future

Case for Change | Aspiration of the Future – Operations Vision





Effective Alarm System

Optimized Control Loops

Safe Operating Limits Managed & Monitored

Effective Operator Situation Awareness

Full Visibility and Control of Safety System Status

Fully Digitalized Logbooks, Permits, Duties, etc.

Actionable KPI's

Layers of Process Safety – Only For Governance?





Process Safety Layers | Measure to Improve





Reference | API 574

- **Conceptually based on the "incident pyramid"**
- □ Identifies leading and lagging process safety indicators to drive performance
- □ Tier 1 is the most lagging, Tier 4 is the most leading
- □ Tiers 1 and 2 are measure of actual releases and may be used for national reporting
- **□** Tiers 3 and 4 are intended for internal or site use

Evacuation Process Relief & Containment Trip/SIS Activation/Unit Shutdown Alarms and Operator Interventions Regulatory Control Loops Procedures and Management Systems

Measuring, understanding, and improving leading indicators (Tier 3 and 4) can prevent Tier 1 and Tier 2 events from occurring

Metrics Drive Actions!

Operational Risk Management

Hexagon Solutions alignment to Layers of Protection Analysis Framework



Hexagon is uniquely positioned to provide the most complete and comprehensive Barrier Management solution to the market.

Link to infographic



Alarm Management Document | Journey of Excellence



HEXAGON

TNChE Asia 2025

Use Case: 1. Alarm Management Analysis Tools





Integrated AEA & D&R = MASTER ALARM DATABASE (MADB)

Analysis:

Start date

End date:

🚾 Frequent Alarms

SAFSHOF

59FI238

61FC159

59A10002

61TI8502

61FC162

68PC101

61FA140

61FA130

61TI8256

59LH525

61AI171

61FA220

61FA120

61FA110

C1EA010

H2SFL

Frequent Alarms

OFFNORI

PVHI

PVLO

PVHI

PVHI

PVLO

PVHI

YES

YES

PVHI

PVLO

YES

YES

YES

VEC

OFFNORM

OFENORM

Document Alarms

- Causes
- Consequences •
- Corrective Actions
- Classification

Classify Alarms

- Process Performance
- Equipment safety
- Your Classification System

Rationalize Priorities

- Impact / Severity / Maximum Response Time
- Priority and Trip Point for each process state
- Template based work process
 - Create templates from any alarm
 - Apply templates to any alarm

Automated Realtime MADB Audit





Use Case: 2. Control Loop Performance Management



Use Case 3. IPL - Safety Lifecycle Management in Operations



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IPL Assurance – Instrument Protective Function

- Improves plant safety and operational awareness of Independent Protection Layer (IPL) performance.
- Optimizes plant resources by automating IPL integrity reporting.
- Provides an audit trail for IEC and OSHA compliance.
- Consolidates important IPL information.



Solution

Comprehensive Solution To Aggregate Information From Disparate Sources To Help Monitor Performance and Visualize Risk

Digitised Safety System Management

IPL Analytics

Configuration and Design Data for Each SIF

Design Time, Process Safety Time, Testing Interval, Risk, Consequence, Severity, SIL Level, etc. Safety System Performance Analysis and Reports

| Analysis Safet | y System Test Sc | helde | | 1 | Parameter | adda): (A.PASTIC) | AGyree | with . | | . 3 | | | | | | | | |
|----------------|--------------------|------------------|-------------|------------|--------------|--------------------|------------|--------------|---------------|----------------|------------|--------|------------|---------------------------|---------------|-----------------|-------|-----------|
| Start date: | | Data con | er Gas Pier | (| Cone | Stone: Selected Au | est: Gas) | Part: Show a | abhrider cont | terits Tue | | | | | | | | |
| Evidate | | Team | | | | | | | | | | | | | | | | |
| Pun Analysis | Custom. | This Morth | The Quer | w) [1 | aat.Year | This Year | Tada; | Las | Month. | Lest Quarter | Yesterday | Last | Days . | | | | | ۲ |
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| 10 | Name | | · Type · | 11 | De | a cription | | Equipment | · Dan Dat | a in Overdan i | Days Orand | ten ∑÷ | Hitigand P | lick = Urenitigated Flick | · Consequence | · Severity · | SIL . | · Protect |
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| + 4215D//005 | | | Bettert | Inlet Co | np. Discher | ge Sdv | - | Compresso | 922214 | Yes | | 675 | | | | | - | |
| 4211/20284 | | | Benet. | Inlet Co. | rup. Seal Ga | s Superheater | | Compresso | 22/2016 | Yes | | 157 | | | | | | |
| 464701 - Sup | enheater Trip | | Function | FUEL G | AS SUPERH | EATER TRIP | | Heaters | 628201 | 6 Yes | | 10 | | | Safley Impact | | | |
| 447P2HH008 | - Filter Inlet Pro | source High High | Function | Filter Inl | et Pressure | High High | | Separators | 628207 | 6 Yes | | 10 | | Minor | | Safey Seventy 3 | | |
| 42150//004 | | | Dament | Inlat Co | np. Suct Sc | rubber Cond. Str. | | Compresso | 628001 | 6 Yes | | 10 | | | | | | |
| 421121.1002 | Soubler Level | Lostav | Function | Stiet Co. | rep Suct Sc | rabber Level Law L | aw. | Compressa | 630/201 | G Yes | | 1 | Major | | | | 51.7 | 1 |
| 443TV101 - M | EG Reboiler | | Benet | Meg Rel | bailer Tv (N | og Regeneration Un | 6 | Bailer | 710916 | Yes | | 7 | | | | | | |
| 4C4330 | | | Benerit | 4:4330 | Fuel Gen Si | oply 5ev | | Pumps | 713/201 | 6 No | | - 6 | | | | | | |
| 421P2LL003 | Pressure Low L | D# | Punction | Inliet Cor | np. Suction | Pressure Low Low | | Compresso | 721201 | 6 No | | -13 | | | | | 58, 5 | 5 (L |
| 42150//007 | | | Detret | Inlet Co | ng: Seal Ga | e Supply (Export C | ias) Sd. | Compresso | 7023001 | 6 No | | -14 | | | | | | |



Process and Event Data from the control system

SIF Activation, Success or Failure Verification, Bypass, Un-Bypass, Test, etc.





Use Case: 4. Boundary Management



New Edit Delete Exp

Inbound – Integrating SDL/SOL/NEL/MDL





Where to Consolidate it? The Master Alarm Database

MADB Capabilities

- Secure, with controlled access
- Create a new section for mapping SIS/SIF/IPLs
- Link to the correct DCS and SIS sensor points for monitoring and analysis
- Correct "single truth" is now in an MOC-controlled environment

Applications Configure Status Window Help | 🏣 🔐 🏠 🐚 🖓 👯 📲 🔕 🕮 🔚 🍇 📐 | 👺 🍑 📑 🔚 🌾 📆 mine Scrubb FAL575 Gire Bfly/Ler FC000 Coboiler Import \square Compresso FC000 🕆 Coolina Towe EC0003 H1 SE COI Debutanize Depropaniz DMC Fluid Varms: 35 Parameters: 6 Environmental Trip Point V+ Approved V+ Y P Alarm Y P State Y P Configured Y P Tag FC0001 PVI I Default NOACTION NOACTION 🔐 H-10 CO00 PVI 0 H-1 Startup Yes NOACTION NOACTION 🕅 General Plar IPI Reliabilit R Heat Med/Slurr H-1 DOWN Yes 250.0000 A Main Air Blowe EC000 PVI 0 250 0000 🕅 Main Frac O Corrective Actio Reactor Coke buildup in the tube Check pressure trends May need to take the coil down for maintenan 🕯 Regen Temp Plugged Straine 2 Regenerato A Solitter Valve malfunctio Check local 🛱 Utility 1 🛱 Utility 2 Consequenc Wet Gas Scrubb Low flow trip of the heater, loss of product 🚞 zDemoDa Greenfield Impact **New Boundary** Constrained By ☑ Constraint Value ☑ Validation w Flow Trip Limit.Defa $\{M\} > \{C\}$ Section 0001 Lower Normal Limit Defau **New IPL** Section HEXAGON

Boundary Excursions are detected, analyzed, and automatically reported.

SIF Activations are detected, analyzed, and automatically reported.

Case Study – Oil & Gas, Refineries, PetroChem Industries Company



- 1. Improve safety by reducing Process alarm per hour per operator and having real time critical data, Managing Bypass and Critical Boundary
- 2. Improve production by monitoring and react on the nonperforming controller

3. Reduce Unplanned Shutdown by reacting to analysis on every Protection Layer as and indication of Performance

 Process Alarm – Loop Performance – Boundary – Safety System Analysis



Policing to Consulting



Digitalization of Reliability and Integrity Management Physical Asset Management of 4 Operational Goals



PRAISe is a integrated physical asset management system that capable to do criticality analysis, reliability & integrity data calculation and ITPM* strategy assessment in a single platform.

| | Reliability & Availability Calculation Module, | FMEA-RCM Module, SCE Identification & SCE SSPS |
|---|---|--|
| • | Management Dashboard Module, | Repository |
| • | Asset Register Module, | Reliability Block Diagram Calculation, |
| | Anomaly Management Module | Life Data Analysis Module |
| | Equipment Criticality Analysis, | And many more |
| | | |
| | | |



Policing to Consulting

| Linetreen | Indianti | ve Dreeses Sefety | Dorfe | | diestore | |
|------------------------|-----------------|---------------------------------|-----------|------------------------|-------------------------|---------------------------------|
| Opstream | inuicati | ve Process Salety | Penc | prmance in | dicators | |
| | | | al Alarms | Average Alarm Rate | Alarm Type | |
| Back to Monthly View | | Ataims | 2,090 | 1 | All 🗸 | |
| Tag | Alarm Alarm Typ | e Point Description | Priorit | y Count Chattering Rep | etitive First Timestamp | |
| TCP2_AI1:B_TI5521 | HIABS Process | TRN 2 1ST STG DISCH TEMP | 3 | 402 | 4/25/2022 6:12:30 AN | |
| B_HOT_OIL:B_LT6400 | LOABS Process | V-507 INTERFACE LEVEL | 2 | 167 | 4/23/2022 9:36:43 PM | |
| B_LP_SEP_ABC:B_LT5070 | HIABS Process | V-507 INTERFACE LEVEL | 2 | 138 | 4/23/2022 2:44:24 PN | |
| 3_OILY_WTR:B_LT5850 | HIABS Process | V-585 INTERFACE LEVEL | 3 | 79 | 4/25/2022 4:53:39 PN | |
| CSDP_CGCE:PZT6031_EN | HIABS Process | PZT-6031 ENGINEERING VALUE | 2 | 43 | 4/23/2022 9:17:50 AN | |
| 489MF_CIN:XS_54320_B | STATE Others | TURBINE1 ENCLSURE COM.AIR 60%LE | L 2 | 42 | 4/23/2022 7:06:56 AN | |
| 489MF CIN:XS 54321 B | STATE Others | VENT EXH 60% LEL | 2 | 42 | 4/23/2022 7:07:00 AN | |
| PRE TREAT:PT6070 | HIABS Process | A6070 CO2 REMV FUEL GAS INLET | 2 | 42 | 4/23/2022 9:17:49 AM | |
| LB WHCP DI1:BPZT04S MC | STATE Others | MOS CNFIRM-WELL B04S HI-LO PILO | T 2 | 39 | 4/23/2022 8:21:41 PM | |
| UEL GAS:PT6030 | LOABS Process | V6030 FG SCRUBBER TO FLTR COALS | 2 | 37 | 4/23/2022 9:36:03 AN | |
| FUEL GAS:PT6030 | HIABS Process | V6030 FG SCRUBBER TO FLTR COALS | 2 | 35 | 4/23/2022 9:17:51 AN | |
| CGCE TCP ALPT2450 | LOABS Process | HPC 1 SUCTION GAS PRESS | 2 | 29 | 4/23/2022 7:06:32 AN | |
| ICP2 AI1:B TI5575 | HIABS Process | TRN 2 2ND STG SUCT TEMP | 2 | 25 | 4/23/2022 2:12:42 PM | |
| CGCE CSDPB PZAHH6075D | STATE Process | PZT-6075 HIGH-HIGH ALARM | 1 | 19 | 4/23/2022 11:17:56 A | |
| CSDP_CGCEPZT6075_EN | HHABS Process | PZT-6075 ENGINEERING VALUE | 1 | 19 | 4/23/2022 11:17:58 A | |
| CP2 DI1:B XI 55311 | STATE Others | GCM TRAIN 2 STOP | 2 | 19 | 4/23/2022 9:40:11 AM | |
| B_SURGE_ABC:B_LT5080 | LOABS Process | V-508 CRUDE LEVEL | 2 | 17 | 4/23/2022 9:23:19 AN | |
| CSDP_CGCE:PZT6075_EN | LLABS Process | PZT-6075 ENGINEERING VALUE | 1 | 17 | 4/23/2022 9:37:04 AM | |
| B HP SEP ABC B LT5041 | LOABS Process | V-504 CRUDE LEVEL | 2 | 14 | 4/23/2022 10:27:43 A | |
| SAS COND:B FT5532 | LOABS Process | SEAL GAS FLOW (SKID 2) | 1 | 14 | 4/23/2022 9:39:13 AM | |
| BOILY WTR B I T5851 | HIARS Process | V=585 CRUDE LEVEL | 2 | 13 | 4/23/2022 10 58 19 A | |
| GCE TCP AIPT2435 | HIABS Process | LPC 2 SUCTION GAS PRESS | - | 10 | ALCOLOLE TO OUT A | |
| GCE TCP AI:PT2436 | LOABS Process | LPC 2 DISCHARGE GAS PRES | Freque | nt alarms ap | pear for consecut | tive weeks. Steps by steps |
| PRE TREAT B PT6071 | LOABS Process | A6070 CO2 REMV FUEL GAS I | | | | |
| CP2 AI1 B PI5521 | LOARS Process | TRN 2 1ST STG DISCH PRESS | trouble | shooting init | iated | |
| CP2 AI1 B PI5575 | LOARS Process | TRN 2 2ND STG SUCT PRESS | | Shooting int | incen. | |
| CD2 DI1-D VI 66201 | CTATE Others | TI IDD 2 IDI C | PRIME | ADB has helr | oed PMA in FARI | Y DETECTION of deformed transmi |
| | Region | Field Year | | | | |
| Legends | PMA | V Dulang V 2022 | V April | ~ | Last Update | |

Creation: RM 700k

Win the Day: ADB - LP Separator Level Transmitter

Approx. Value Creation: RM 700k



Win the Day: IPM – High SCE Bypass

Approx. Value Creation: USD 10mil

- 29 prolonged bypasses has been identified during bi-weekly sitting of Offshore platforms.
- Collaboration between Instrument, Frontliners, Asset team, Process Technologist to chart way forward for each tags.
- 17 bypassed has been normalized related to current operating and parameter and setpoints.
- 12 SSBOC with details discussion between SMES, PTS-PSM and Operations.



Policing to Consulting

Process Safety KPI

[Open]

PSPI KPI Reporting Flow

Manual PSPI Management Reporting

Process Owner : Process Safety Engineer, Prod Supt., Instrument Technician, Instrument Engineer, HSE Process Safety Engineer

| | | PSPI Reporting Process | | | | | | | | | | | |
|----|-------------------------------------|----------------------------------|---------------------------|-----------|------------------|-----------------------------------|-------------|--------------|------------------|----------------------------------|-------------------------------|------------|------------------|
| No | Required Data Input | | Data Co | llection | | C | ata Process | ing & Analys | sis | | Output 0 | Collection | \frown |
| | | Method | PIC | Lead Time | Accuracy | Method | PIC | Lead Time | Accuracy | Method | PIC | Lead Time | Accuracy |
| 1 | Average Alarm/hour/operator | Manual Extraction from DCS | Prod Supt / Instr Tech | 2.0 | Accurate | Manual analysis using Excel | Instr Eng | 2 dava | Less Accurate | Manual Collection from PIC | Process Safety Engineer | | Less Accurate |
| 2 | Peak Alarm rate/10 minutes | Manual Extraction from DCS | Prod Supt / Instr Tech | 5 Days | Accurate | Munual analysis using Excel | Instr Eng | 5 days | Less Accurate | Manual Collection from PIC | Process Safety Engineer | | Less Accurate |
| 3 | IPF Fail on demand | Manual Extraction from DCS | Prod Supt / Instr Tech | | Less Accurate | Manual analysis using Excel | Instr Eng | | Less Accurate | Manual Collection from PIC | Process Safety Engineer | 1 Day | Less Accurate |
| 4 | IPF activation on demand | Manual Extraction from DCS | Prod Supt / Instr Tech | 2 Days | Accurate | Manual ana ysis using Excel | Instr Eng | 1 Day | Accurate | Manual Collection from PIC | Process Safety Engineer | | Accurate |
| 5 | NEL Excursion | Manual Extraction from DCS | Prod Supt / Instr Tech | | Less Accurate | Manual analysis using Excel | Instr Eng | | Less Accurate | Manual Collection from PIC | Process Safety Engineer | | Less Accurate |
| | TOTAL LEAD TIME & ACCURACY LEVEL | | | 6 Days | Less Accurate | | | 4 Days | Less Accurate | | | 1 Day | Less Accurate |

Process Safety KPI Reporting from 9 days to 1 day with accuracy and validated data – via Hexagon PSI

Process Owner : Process Safety Engineer, Prod Supt., Instrument Technician, Instrument Engineer, HSE Process Safety Engineer

| | | PSPI Reporting Process | | | | | | | | | | | | |
|----|------------------------------------|--|-------------------------------|-----------|----------|--|----------------------------|-----------|----------|--|--|-----------|----------|--|
| No | Required Data Input | | Data Co | llection | | D | Data Processing & Analysis | | | | Output Collection | | | |
| | | Method | System | Lead Time | Accuracy | Method | PIC | Lead Time | Accuracy | Method | PIC | Lead Time | Accuracy | |
| 1 | Average | | | | | | | | | | | | | |
| | A larm/hour/operator | | | | | | | | | | | | | |
| 2 | Peak Alarm rate/10 | | | | | | | | | Manual | Process | | | |
| | minutes | Automatic data capturing from DCS | | Real Time | Accurate | Automatic Analysis using Software | PRIME | Real Time | Accurate | Analysis Using PRIME report/Dash board | Safety Engineer/HS E Process Safety Engineer | 1 Day | | |
| 3 | IPF Fail on demand | | data capturing from DCS | | | | | | | | | | Accurate | |
| 4 | IPF activation on demand | | | | | | | | | | | | | |
| 5 | NEL Excursion | | | | | | | | | | | | | |
| Т | OTAL LEAD TIME & ACCURACY LEVEL | | | Real Time | Accurate | | | Real Time | Accurate | | | 1 Day | Accurate | |



Plant Digital Data Model Structure Overview





Components of Operational and Maintenance Management - VISION

3 Take-aways

- **Practical Digitalization** Hexagon can help customers expand and interconnect their digitalization, unlocking new potential for their business and increasing potential benefits through a holistic and integrated approach.
- Interoperability Centralize and visualize all types of asset information from data historians, the CMMS, the DCS, EAM, PLC and SCADA systems.
- Smart Digital Reality Bringing It All Together Using our Smart Digital Reality, you can deploy a comprehensive digital twin with Current Technology that enables an information management data ecosystem that's built and maintained throughout the asset lifecycle, allowing for a continuous journey of operational excellence.







Come and visit us at Booth D6!

